

1 **Dissecting the Role of Substrate on the Morphology and Separation**  
2 **Properties of Thin Film Composite Polyamide Membranes: Seeing is**  
3 **Believing**

4 Lu Elfa Peng,<sup>†</sup> Zhikan Yao,<sup>‡</sup> Zhe Yang,<sup>†</sup> Hao Guo,<sup>\*,†</sup> Chuyang Y. Tang<sup>\*,†</sup>

5

6 <sup>†</sup>Department of Civil Engineering, The University of Hong Kong, Pokfulam, Hong Kong  
7 SAR, China.

8 <sup>‡</sup>College of Chemical and Biological Engineering, Zhejiang University, Hangzhou, 310027,  
9 China.

10

11

12

13

14

15

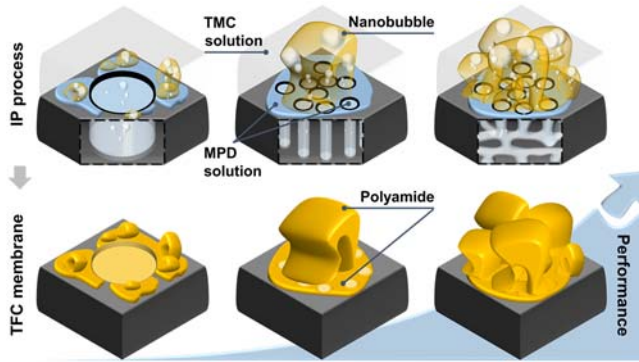
16 \*Corresponding Authors:

17 Hao Guo, [guohao7@hku.hk](mailto:guohao7@hku.hk), +852 28578470

18 Chuyang Y. Tang, [tange@hku.hk](mailto:tange@hku.hk), +852 28591976

19

20 **TABLE OF CONTENT**



21

22

23

24 **ABSTRACT**

25 Recent studies show that the surface morphology of a thin film composite (TFC) polyamide  
26 membrane depends strongly on its porous substrate. Nevertheless, the underlining  
27 mechanisms and the effects on membrane separation performance remain controversial.  
28 To dissect the exact role of pore properties, we synthesized TFC polyamide membranes on  
29 polycarbonate substrates with cylindrical track-etched pores (PCTE) of well-defined pore  
30 size ranging from 10 to 800 nm. Leaf-like roughness features were most prominent for  
31 polyamide films formed on substrates of intermediate pore sizes (80 and 100 nm). Smaller  
32 pores inhibited leaf-like features as a result of insufficient storage of *m*-phenylenediamine  
33 (MPD) monomers for the interfacial reaction, whereas larger pores resulted in diminished  
34 surface roughness due to the lack of confinement to the interfacially degassed nanobubbles.  
35 Substrate porosity plays a critical role on membrane water permeability, while smaller  
36 pores with greater pore density are favored to improve membrane rejection. TFC  
37 polyamide membranes prepared on sponge-like polyethersulfone and polysulfone  
38 substrates exhibit better water permeability and salt rejection compared to the PCTE-TFC  
39 membranes, thanks to the simultaneously enhanced confinement and MPD storage effects.  
40 The mechanistic insights gained in this study reveals the huge potential of substrate design  
41 towards high performance TFC RO membranes.

42 **INTRODUCTION**

43 Researchers have been constantly questing for reverse osmosis (RO) membranes of better  
44 permeability and higher selectivity<sup>1-4</sup> to make them more competitive for desalination and  
45 water reuse.<sup>5-8</sup> Commercial RO membranes are generally prepared by an interfacial  
46 polymerization (IP) reaction between *m*-phenylenediamine (MPD) dissolved in water and  
47 trimesoyl chloride (TMC) dissolved in an organic solvent. Typically, a porous substrate  
48 saturated with MPD is brought into contact with the organic solution of TMC, which forms  
49 a thin cross-linked polyamide rejection film. Traditional wisdom often discounts the  
50 importance of substrate based on the simple belief that membrane separation performance  
51 is governed by the polyamide layer.<sup>9-11</sup> Nevertheless, recent studies revealed its critical  
52 influence on the morphology of the polyamide film<sup>12-14</sup> as well as its role in governing the  
53 hydraulic transport path within the composite membrane.<sup>15-17</sup> Improved membrane  
54 substrates have the potential to achieve an order of magnitude improvement in water  
55 permeability while maintaining the salt rejection.<sup>18, 19</sup>

56

57 Increasing number of studies have reported the influence of substrate properties (e.g. pore  
58 size,<sup>12, 15, 20</sup> pore density,<sup>14</sup> porosity,<sup>13, 21, 22</sup> and hydrophilicity<sup>12, 21</sup>) on the polyamide  
59 morphology. Nevertheless, their exact roles remain controversial. Several studies observed  
60 increased membrane surface roughness using substrates with larger pores,<sup>12, 23, 24</sup> yet others  
61 reported an opposite trend.<sup>13, 18, 22</sup> The effect of substrate on membrane separation  
62 performance is equally confusing. Singh et al.<sup>15</sup> reported that increasing the substrate pore  
63 size from 70 nm to 150 nm led to a thicker polyamide film with reduced water permeability.  
64 In contrast, Ghosh et al.<sup>12</sup> obtained more permeable membranes for relatively hydrophobic

65 substrates with larger pore diameters. These authors proposed a “volcano eruption” model  
66 to rationalize their results, i.e., a larger pore favors the eruption of its stored MPD, whose  
67 reaction with TMC forms a rough polyamide film spanning over the pore. Increased  
68 number of studies have also investigated the effect of surface porosity and pore density of  
69 the substrate.<sup>13, 14, 16, 21, 22, 25</sup> Furthermore, existing studies generally adopt substrates with a  
70 sponge-like skin, whose irregular surface pore structure complicates the decoupling of the  
71 individual effects of various substrate properties. These apparent deficits prompt us to  
72 perform a more systematic investigation to unveil the fundamental mechanisms governing  
73 the role of substrates.

74

75 Recent studies on advanced membrane characterization and formation mechanism of  
76 polyamide may provide us some useful hints. The polyamide film, with an apparent  
77 thickness on the order of 100 nm,<sup>26-28</sup> contains numerous nanovoids<sup>29-31</sup> such that its  
78 intrinsic thickness is as thin as 10-30 nm.<sup>25, 32-34</sup> Ma et al.<sup>35, 36</sup> revealed that these nanovoids  
79 are caused by interfacial degassing due to the release of H<sup>+</sup> and heat during the IP reaction.  
80 That is, the localized acidification and heating at the IP reaction interface converts the  
81 bicarbonate in the MPD solution (see Supporting Information S4) into CO<sub>2</sub> nanobubbles  
82 ( $\text{HCO}_3^- + \text{H}^+ \xrightarrow{\Delta} \text{CO}_2\uparrow + \text{H}_2\text{O}$ ). These nanobubbles are encapsulated within the polyamide  
83 film, which forms its “leaves and nodules” morphology.<sup>25, 35-37</sup> Song et al.<sup>38</sup> further  
84 demonstrates the importance of confinement conditions: the roughness features of leaves  
85 and nodules disappeared for polyamide films prepared at a free interface. The lack of  
86 substrate in this case allows the degassed nanobubbles to freely escape from the interface,  
87 in contrast to the conventional case that nanobubbles are confined between the substrate

88 and the polyamide film. Presumably, the confinement effect will be significantly weakened  
89 with larger substrate pore size (e.g., a free interface can be idealized as a substrate with  
90 infinitely large pore size), which can provide a new and unique angle to interpret the role  
91 of substrates.

92

93 To dissect the role of substrates on the formation of polyamide morphology, we selected  
94 polycarbonate membranes with track-etched cylindrical pores (PCTE). Additional  
95 substrates were also included for comparison purpose, including polyethersulfone (PES)  
96 and polysulfone (PSf) substrates prepared by phase inversion, and nanofibrous  
97 polyacrylonitrile (PAN) substrate prepared by electrospinning. We carefully characterized  
98 the membrane morphology and separation properties, which provides deep insights on the  
99 critical role of substrate during IP reaction.

100

101 **MATERIALS AND METHODS**

102 **Chemicals and membrane substrates.** Chemicals used for membrane preparation,  
103 including MPD (99%), TMC (98%), n-hexane (HPLC grade), PSf (Mw ~ 35000), and  
104 dimethylformamide (DMF, anhydrous 99.8%) were all obtained from Sigma-Aldrich.  
105 Other chemicals, including tetrahydrofuran and sodium chloride (NaCl) were purchased  
106 from Dieckmann. PCTE were supplied by Sterlitech. These substrates have uniform  
107 cylindrical pores, with nominal pore size ranging from 10 to 800 nm. They are denoted as  
108 PCTE-10 to PCTE-800 in accordance to their nominal pore size. Other commercial  
109 substrates used in this study include a nanofibrous PAN prepared by electrospinning  
110 (Sterlitech) and two PES substrates prepared by phase inversion (PES1 from Synder and  
111 PES2 from Sterlitech). An additional PSf substrate was prepared in-house by phase  
112 inversion as described in our previous works.<sup>37, 39</sup> Detailed properties of these substrates  
113 are summarized in Table 1.

114

115 **Fabrication of TFC polyamide RO membranes.** TFC membranes were prepared by  
116 performing IP reaction on various substrates. Briefly, a substrate was first soaked in 1 wt. %  
117 aqueous MPD solution for 2 min. After removing excess MPD solution by a rubber roller,  
118 a 0.1 wt. % TMC/hexane solution was applied to the MPD-impregnated substrate for 1 min  
119 to form polyamide. The resultant polyamide membrane was rinsed by hexane and kept in  
120 50 °C water bath for 10-min for further polymerization. The TFC membranes formed on  
121 PCTE substrates are denoted as TFC-10 to TFC-800 based on the nominal pore size of the  
122 substrates, and those made on commercial/homemade substrates are named as TFC-PES1,  
123 TFC-PES2, TFC-PSf, and TFC-PAN according to the type of substrate used.

124

125 **Membrane characterization.** Field-emission scanning electron microscopy (FE-SEM, S-  
126 4800, Hitachi) was used to characterize membrane morphology. All SEM samples were  
127 dried and sputter-coated with a thin layer of gold. To obtain the bottom surface of the  
128 polyamide layer, the substrate was removed by gently dripping a suitable solvent, i.e.,  
129 tetrahydrofuran for dissolving PCTE or DMF for dissolving PES, PSf, and PAN. The  
130 isolated polyamide layer was placed on a silicon wafer with bottom surface-side up and  
131 thoroughly dried before further characterization.

132

133 **Membrane separation performance.** Membrane performance including water flux and  
134 salt (NaCl) rejection were tested using a laboratory-scale cross-flow RO filtration system  
135 as detailed in the previous work.<sup>37</sup> The effective filtration area of each membrane coupon  
136 was 12.0 cm<sup>2</sup>. After pre-compaction at 17.0 bar for 2 h, the membrane coupon was tested  
137 using a 2000 ppm NaCl feed solution at 15.5 bar with a cross-flow velocity of 22.4 cm/s  
138 under room temperature (~25 °C). The water flux  $J_v$  and permeability  $A$  are calculated by:

139 
$$J_v = \frac{\Delta m}{\Delta t \times a \times \rho} \quad (1)$$

140 
$$A = \frac{J_v}{\Delta P - \Delta \pi} \quad (2)$$

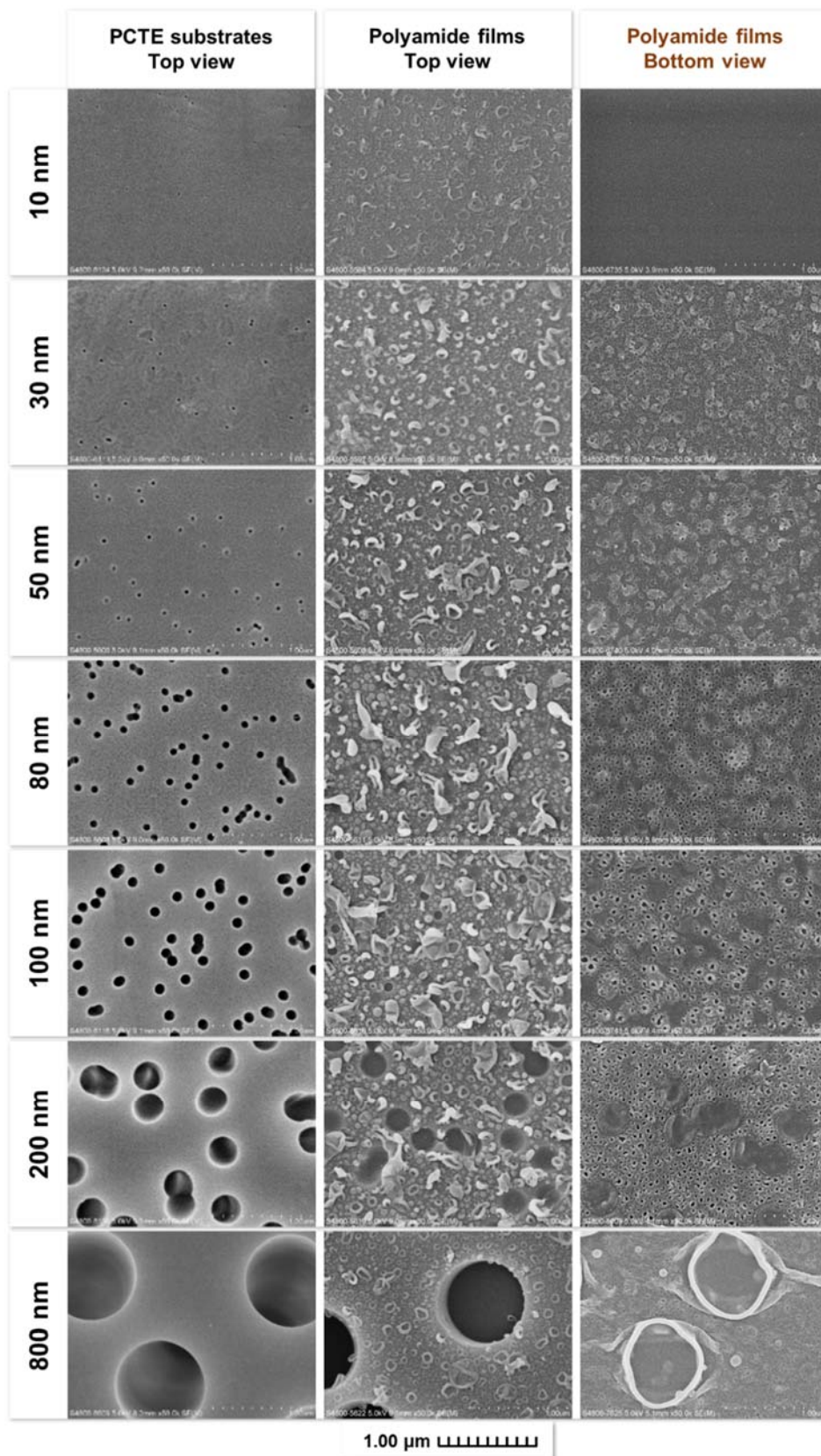
141 where  $\Delta m$  is the mass of permeate over a time interval of  $\Delta t$ ,  $a$  is the effective membrane  
142 area,  $\rho$  is the density of water,  $\Delta P$  is the transmembrane pressure, and  $\Delta \pi$  is the  
143 transmembrane osmotic pressure.



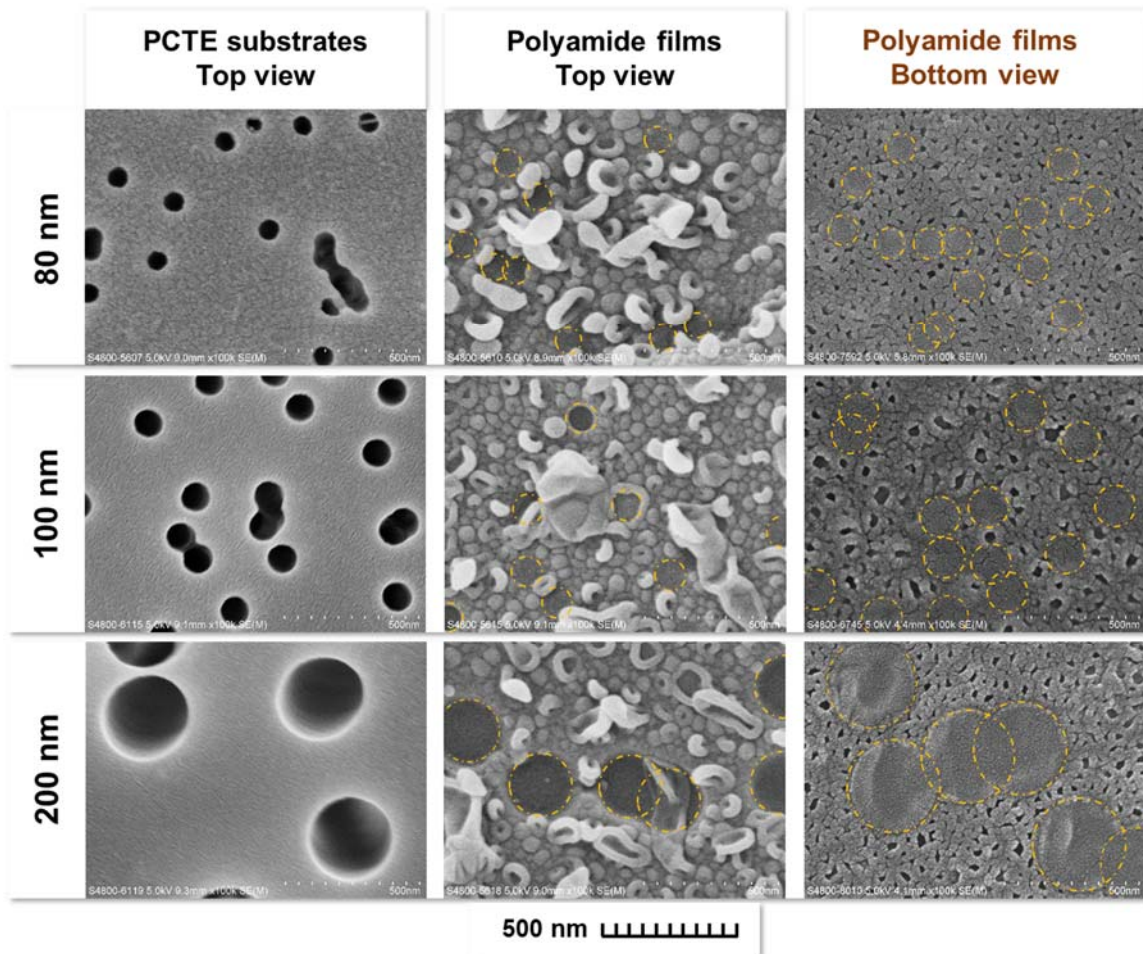
144 NaCl concentrations in the feed and the permeate (i.e.,  $C_f$  and  $C_p$ , respectively) were  
145 determined based on conductivity measurements (Ultrameter II, Myron L). NaCl rejection  
146 ( $R$ ) was calculated by:

$$147 \quad R = \frac{C_f - C_p}{C_f} \times 100\% \quad (3)$$

148



151 **Figure 1.** SEM micrographs of the PCTE substrates and the top and bottom views of polyamide films  
 152 for the corresponding TFC membranes. Scale bar = 1.00  $\mu\text{m}$ .  
 153



154  
 155 **Figure 2.** Magnified SEM micrographs of PCTE substrates surface (PCTE-80, PCTE-100, and PCTE-  
 156 200) and the top and bottom views of polyamide films for the corresponding TFC membranes (TFC-80,  
 157 TFC-100, and TFC-200). Scale bar = 500 nm.  
 158  
 159

160 **Table 1.** Properties of substrates used in the current study.

	PCTE							PES1	PSf	PES2	PAN
Nominal size <sup>a</sup>	10 nm	30 nm	50 nm	80 nm	100 nm	200 nm	800 nm	300 kDa	NA	30 nm	200 nm
Observed size (in diameter) (nm) <sup>b</sup>	13 ± 4	28 ± 2	40 ± 5	72 ± 6	106 ± 4	270 ± 12	890 ± 20	16 ± 4	35 ± 12	186 ± 122	NA
Pore density (counts/μm <sup>2</sup> ) <sup>b</sup>	8 ± 1	5 ± 1	10 ± 2	14 ± 1	11 ± 1	4 ± 1	1 ± 1	307 ± 55	325 ± 16	8 ± 2	NA
Surface porosity (%) <sup>b</sup>	0.1	0.4	2.0	7.2	8.6	8.6	25.1	6.2	31.3	21.2	NA

161 Note:

162 a. Provided by manufacturer.

163 b. Based on SEM characterization (see more details in Supporting Information S1).

164

165 **TFC membranes formed on PCTE.** Figure 1 presents the SEM micrographs of the PCTE  
 166 substrates (top view) and the polyamide films (both top and bottom views). It is important  
 167 to note that the actual pore size of PCTE-200 and PCTE-800 was approximately 70 - 90  
 168 nm larger than the respective nominal sizes provided by the manufacturer (Table 1). The  
 169 nominal size of other PCTE substrates were reasonably accurate. The top surfaces of  
 170 polyamide films show leaf-like roughness features, whose presence were most obvious for  
 171 TFC-80 and TFC-100. Increasing the substrate pore size from 100 nm to 800 nm led to the  
 172 diminishing of these characteristic features. According to our recent works,<sup>35</sup> the leaf-like  
 173 features were formed due to the interfacial degassing of CO<sub>2</sub> nanobubbles that are  
 174 encapsulated between the polyamide film and the substrate. Increasing the pore size of the  
 175 substrate would reduce the confinement effect by the substrate and allow the nanobubbles  
 176 to escape through the large pores.<sup>38</sup> In contrast to the common belief that leaves grow  
 177 directly over pores,<sup>12, 20</sup> we observed smooth and flat polyamide films spanning over the  
 178 pores of 80-200 nm (highlighted by dotted circles in Figure 2). Indeed, the leaf-like features  
 179 developed predominantly around the pores. Although these observations appear to be

180 peculiar and counter-intuitive, they are consistent with the interfacial degassing theory.<sup>35</sup>  
181 <sup>37,38</sup> Due to the release of heat and H<sup>+</sup> during the IP reaction, the dissolved bicarbonate will  
182 be degassed (see ref.<sup>37</sup> and Supporting Information S4). This degassing can possibly  
183 happen both inside the substrate pores and at the vicinity of the pores. The confinement  
184 effect by the solid matrix around the pores allows the CO<sub>2</sub> nanobubbles to be retained,  
185 which shapes the leaf-like roughness features.<sup>38</sup> However, the confinement effect was the  
186 weakest directly over the straight cylindrical pores, which prevents the effective retention  
187 of degassed nanobubbles. Therefore, our study further confirms the critical importance of  
188 the substrate confinement effect in shaping the polyamide surface roughness. This  
189 confinement effect also explains why surface roughness could not effectively develop for  
190 polyamide films formed at free interfaces.<sup>32,38,40</sup> With a further increase of substrate pore  
191 size to 800 nm, the polyamide intruded into the substrate due to a lack of effective support  
192 (see the bottom view of TFC-800 in Figure 1).

193

194 Interestingly, increasing the substrate pore size from 10 to 80 nm led to an opposite trend.  
195 While the roughness features were barely noticeable for TFC-10, they became increasingly  
196 larger for TFC-30, TFC-50 and TFC-80. This trend can possibly be rationalized by the  
197 greater storage of MPD (Supporting Information S4) and its enhanced diffusion with the  
198 increasing pore size.<sup>13,15</sup> According to the interfacial degassing theory, increasing the  
199 effective concentration of MPD would cause greater production of heat at the reaction  
200 interface to promote the release of CO<sub>2</sub> nanobubbles.<sup>35</sup> Our observation is also consistent  
201 with some earlier studies reporting increased roughness formation for larger pores.<sup>12,23,24,</sup>  
202 <sup>40</sup> Some of the earlier studies attributed the greater roughness to the enhanced “volcanic”

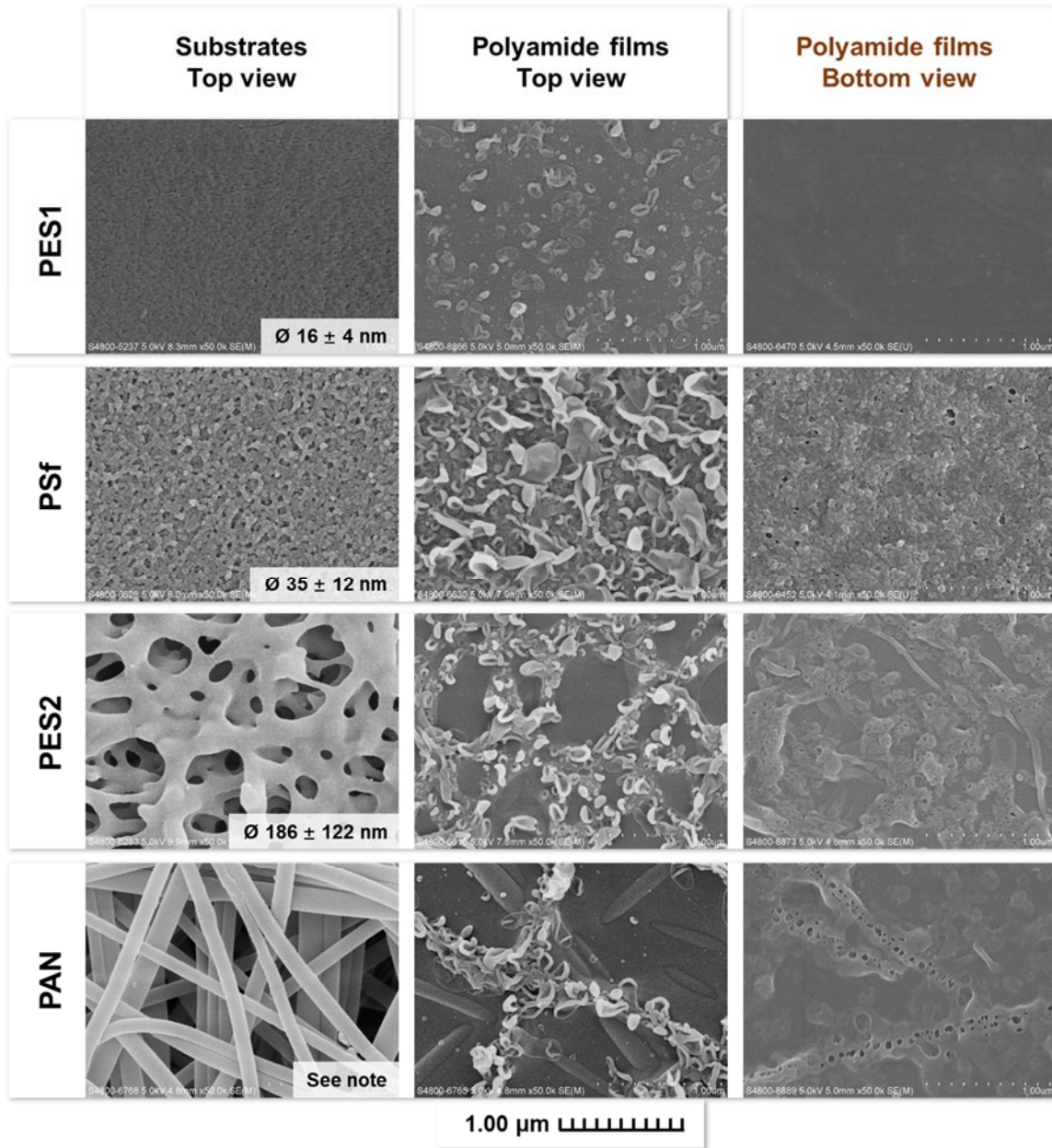
203 eruption of MPD.<sup>12, 41, 42</sup> However, this eruption model alone (which would predict the  
204 greatest roughness for TFC-800 as well as the formation of roughness features directly over  
205 pores) cannot fully explain the surface morphology of the polyamide film. In the current  
206 study, we demonstrate that this surface morphology is governed by two competing  
207 mechanisms, with larger pores leading to reduced confinement effect (a roughness inhibitor)  
208 in addition to greater MPD storage (a roughness promoter).

209

210 Consistent with previous reports,<sup>22, 25, 38, 43</sup> we observed “honeycomb-like” pore openings  
211 over the bottom side of the polyamide films (Figure 1 and Figure 2). The size and number  
212 density of these openings (Table S1) appear to be well correlated to the surface roughness.  
213 For example, TFC-80 had the greatest number density ( $323 \pm 30$  counts/ $\mu\text{m}^2$ ), which was  
214 approximately an order of magnitude higher than that of TFC-30 and TFC-800. For the  
215 case of TFC-10, such back-side openings cannot be clearly identified. According to Song  
216 et al.,<sup>25, 38</sup> the growth of nanobubbles shapes the surface roughness of the film, while their  
217 forced escape from the backside of the polyamide leaves the “honeycomb-like” openings  
218 behind. It is interesting to note the absence of such openings for polyamide formed directly  
219 over the large substrate pores where the confinement effect was the weakest (TFC-80,  
220 TFC-100 and TFC-200, Figure 2).

221





222

223 **Figure 3.** SEM micrographs of commercial/homemade substrates and the top and bottom views of  
 224 polyamide films of the corresponding TFC membranes (TFC-PES1, TFC-PSf, TFC-PES2 and TFC-  
 225 PAN). Scale bar = 1.00 µm. Note: the electrospun PAN substrate had less well-defined pores with  
 226 irregular shape.

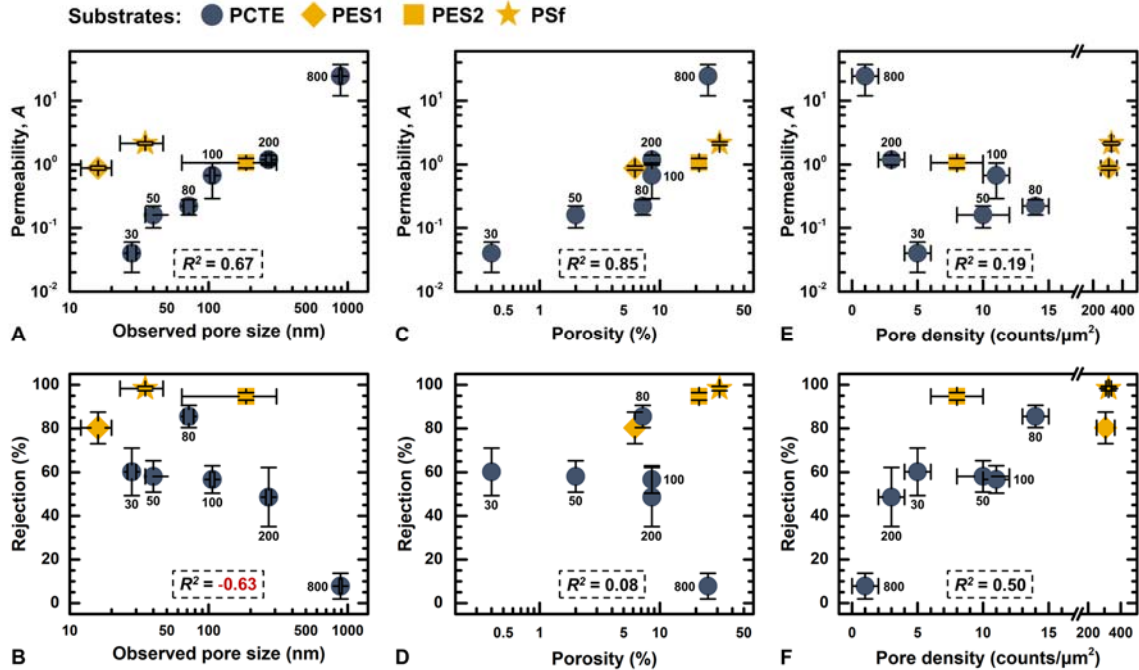
227

228 **TFC membranes formed on other substrates.** Figure 3 presents SEM micrographs of  
 229 TFC membranes prepared on other types of substrates, i.e., PES1, PSf, PES2 and PAN in  
 230 increasing surface pore size. Consistent with the results for PCTE substrates, roughness

231 features could not effectively develop directly over large pores ( $\gg 100$  nm) of the  
232 electrospun nanofibrous PAN. Similarly, leaf-like features could not be found over the  
233 large pores of PES2 (prepared by conventional phase inversion). These observations  
234 further underpin the role of confinement on roughness formation. Indeed, the leaf-like  
235 features of TFC-PES2 and TFC-PAN concentrated over the solid polymeric regions of their  
236 substrates where the confinement effect would be the strongest. The PSf substrate, with an  
237 average pore size of  $35 \pm 12$  nm, had the most prominent “leaves and nodules” appearance.  
238 In contrast, PES1 with smaller pore size presents smaller roughness features, possibly due  
239 to the reduced storage of MPD. In addition to the substrate pore structure, other factors  
240 such as the surface hydrophilicity, morphology and specific chemistry of the substrate may  
241 not neglected.<sup>12, 44, 45</sup> For example, increased substrate hydrophobicity appears to reduce  
242 the formation of leaf-like roughness features (Supporting Information S3), which is likely  
243 due to reduced capillary effect and thus reduced MPD uptake by the substrate. Furthermore,  
244 the use of some specific chemistry may also significantly increase the MPD uptake (e.g.,  
245 due to hydrogen bonding).<sup>19, 46</sup> Future studies on the influence of the surface roughness of  
246 the substrate on polyamide morphology is also needed.

247





248

249 **Figure 4.** Correlations between pore properties of substrates with the separation performance of the  
 250 TFC membranes. Note: TFC-10 did not show any water permeability. On the other hand, TFC-PAN  
 251 had nearly zero rejection against NaCl, implying the failure to form an intact rejection layer. Therefore,  
 252 these two membranes were excluded from the correlation analysis. PCTE substrates are labeled using  
 253 the corresponding nominal pore size, while the measured pore size (Table 1) is used in the figure.  $R^2$  is  
 254 the correlation coefficient obtained from Microsoft Excel between separation properties (rejection or  
 255  $\log(\text{permeability in } \text{Lm}^{-2}\text{h}^{-1}\text{bar}^{-1})$ ) and pore properties ( $\log(\text{pore size})$ ,  $\log(\text{porosity})$ , or pore density).

256

257 **Effect of substrate pore properties on membranes separation performance.** Figure 4

258 presents the effect of substrate pore size, porosity and pore density on the permeability and

259 rejection of the TFC membranes. For the PCTE substrates, increasing substrate pore size

260 had an obvious positive effect in increasing the TFC membrane permeability (Figure 4A).

261 However, the membrane rejection can be seriously comprised for cylindrical pores of

262 greater than 100 nm in size (Figure 4B), possibly due to the greater tendency to form more

263 defects in the polyamide layer over large substrate pores.<sup>19</sup> In addition, for the ultrathin and

264 supported polyamide film that spans over the large cylindrical pores of PCTE substrates, it

265 is mechanically unstable (e.g., the thin film is stretched due to the tensile stress in

266 longitudinal direction when the membrane is pressurized, causing a loss of membrane

267 integrity<sup>47, 48</sup>). Compared to the PCTE counterparts, the corresponding PES and PSf  
268 substrates with comparable pore sizes showed better combinations of permeability and  
269 rejection, implying that substrates with sponge-like structures are preferred for interfacial  
270 polymerization. Notably, the much improved permeabilities of TFC-PES1 and TFC-PSf  
271 (average substrate pore sizes of  $16 \pm 4$  nm and  $35 \pm 12$  nm, respectively) over their TFC-  
272 PCTE counterparts of similar pore size range (10-50 nm) can be explained by the  
273 substantially higher surface porosity for sponge-like substrates. Indeed, Figure 4C shows a  
274 much better correlation between permeability and porosity ( $R^2 = 0.85$ ), revealing substrate  
275 surface porosity as a more important parameter than pore size in governing the permeability  
276 of the resulting TFC membrane. Our work is in good agreement with the existing literature  
277 that high-porosity substrates are favored to reduce the hydraulic resistance for water  
278 transport through the polyamide layer.<sup>14-17</sup> In the current study, the correlation between the  
279 TFC permeability and substrate pore density ( $R^2 = 0.19$ ) was much weaker (Figure 4E).

280

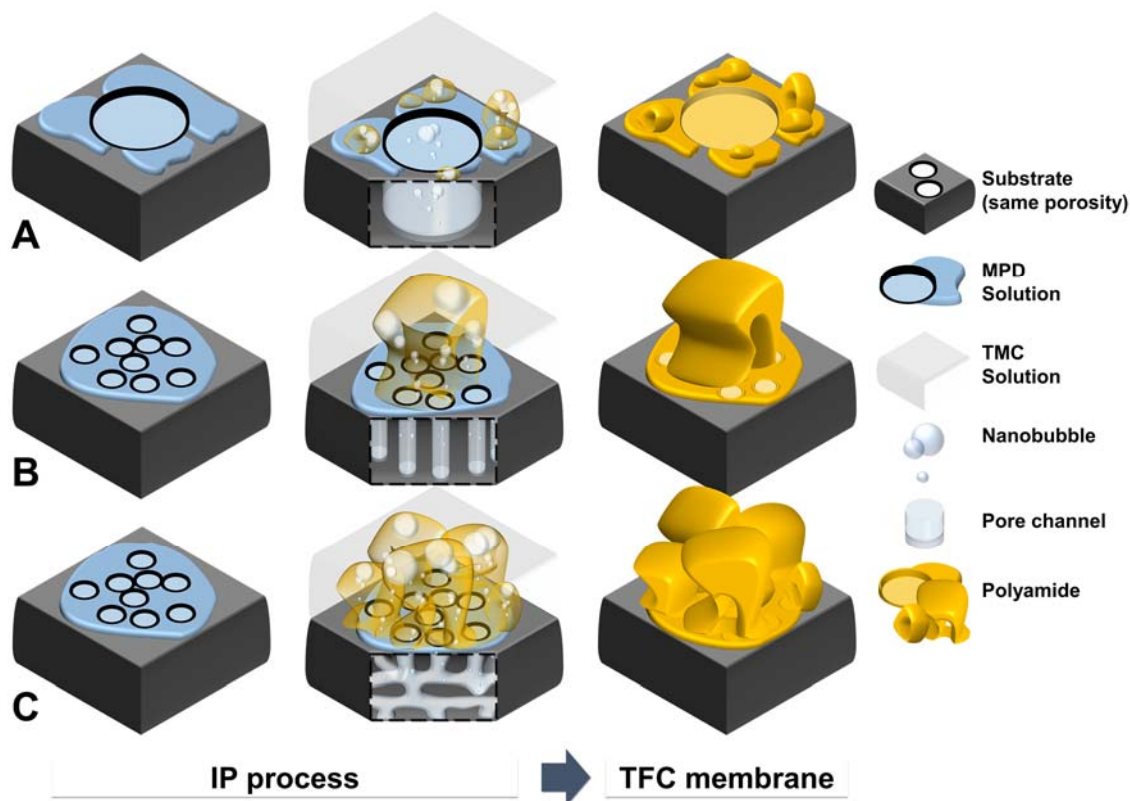
281 Despite the overall good correlation between membrane permeability and substrate  
282 porosity, it is important to note its inherent limitations. For example, TFC-800 had a very  
283 low NaCl rejection of  $< 10\%$ , which was likely caused by either defects formed during  
284 membrane formation or mechanical damages due to the applied pressure during membrane  
285 testing. These defects or mechanical damages may lead to artificially increased  
286 permeability (Supporting Information S5), which possibly explains why TFC-800 deviates  
287 significantly from the overall trend established by the other datapoints in Figure 4C.  
288 Furthermore, the much improved permeabilities of TFC-PES1 and TFC-PSf over their  
289 TFC-PCTE counterparts of similar pore size range may not be completely explained by the

290 substantially higher surface porosity for sponge-like substrates, since membrane  
291 permeability can also be potentially affected by the type of materials and pore morphology.  
292 Future studies are needed to further investigate these factors.

293

294 Unlike membrane permeability that shows the greatest dependence on substrate porosity  
295 ( $R^2 = 0.85$ , Figure 4C), the dependence of rejection on substrate porosity was more  
296 disparate ( $R^2 = 0.08$ , Figure 4D). While some high-porosity TFC-PCTE membranes  
297 suffered from low rejections, increasing porosity appears to enhance rejection for  
298 membranes prepared on sponge-like PES and PSf substrates. In general, membranes  
299 formed on PES and PSf had much higher rejection than TFC-PCTE membranes. For the  
300 PCTE substrates, higher porosity was mainly due to the increased pore size (Table 1). For  
301 the PES and PSf substrates, increasing porosity can be achieved by the combination of  
302 greater pore size and higher pore density. In the current study, larger pore size tends to  
303 cause lower rejection (Figure 4B) while greater pore density favors better rejection (Figure  
304 4F).

305



306

307

308 **Figure 5.** Conceptual illustration of the role of substrate on interfacial polymerization.

309

310 **Mechanistic insights and future perspectives.** The current study highlights two  
 311 important roles of the substrates during the formation of polyamide rejection films: the  
 312 storage of MPD monomers and the provision of confinement to interfacially degassed  
 313 nanobubbles. Although increasing pore size is favorable to increase the MPD storage  
 314 (Supporting Information S4), it results in a simultaneous loss of the confinement effect  
 315 (Figure 5A). For example, even though the amount of dissolved CO<sub>2</sub> in the PCTE-800  
 316 substrate was nearly double of that in the PSf substrate (Supporting Information S4),  
 317 PCTE-800 was less effective to form roughness features over its large sized pores (Figure  
 318 1). For such substrates containing pores, nodules and leaf-like features appeared  
 319 predominately over the solid polymeric areas adjacent to the pore region. According to our

320 prior studies, confined nanobubbles tend to deliver MPD monomers to the reaction front  
321 due to the convection under a pressure gradient, which favors the sealing of defects in  
322 polyamide films formed under mild interfacial degassing.<sup>25</sup> In contrast, the lack of  
323 confinement results in polyamide films with more defects and lower salt rejection.<sup>38</sup> In  
324 addition to the loss of confinement, large substrate pores may further lead to undesirable  
325 intrusion of polyamide into the substrate pores (Figure 2 and Ref.<sup>19</sup>). Thin films spanning  
326 over larger unsupported distance are also less mechanically stable, especially under high  
327 applied mechanical pressure.<sup>47</sup>

328

329 Our study further implies that substrates with greater number of smaller pores are favored  
330 over those with fewer numbers of larger pores in order to achieve better salt rejection  
331 without sacrificing permeability. In this combination, the large pore density helps to  
332 maintain the desired surface porosity (thus MPD storage during the interfacial reaction and  
333 path for water permeation in the resultant membrane), and the smaller substrate pore size  
334 ensures proper confinement effect and high membrane rejection (Figure 5B).  
335 Coincidentally, a modelling work by Ramon et al.<sup>16</sup> also suggested that greater number of  
336 smaller pores are more favorable to minimize the average transport distance through the  
337 polyamide film, noting that their work implicitly assumes that the formation of polyamide  
338 film itself is not affected by the substrate pore structures. Our work demonstrates that,  
339 although nodules and leaf-like features cannot be effectively developed over large pores of  
340 ~ or > 100 nm, these roughness features can be formed over smaller pores as a result of  
341 stronger confinement effect. For densely packed small pores, it is likely that a cluster of  
342 neighboring substrate pores act together for the formation of roughness features. That is,

343 MPD is released from these pores, whose reaction with TMC forms degassed nanobubbles  
344 that are effectively retained by the substrate (due to the greater resistance to air passage  
345 with the presence of solid regions and smaller pore size) to shape the formation of  
346 roughness features. This hypothesis is supported by several recent studies: (1) microscopic  
347 characterization of commercial TFC membranes reveals that each roughness nodule spans  
348 over multiple substrate pores,<sup>20, 25, 38</sup> and (2) tracer filtration tests confirm that the  
349 nanovoids contained in roughness nodules are directly connected to the substrate pores.<sup>25,</sup>

350 <sup>49</sup>

351

352 Although this study used PCTE substrates to dissect the role of substrate pores, the TFC  
353 membranes prepared on conventional PES and PSf substrates showed much better  
354 combinations of permeability and rejection, underpinning the preference of substrates with  
355 higher porosity, greater pore density yet smaller pore size. In addition, PES and PSf  
356 substrates could further enhance the MPD storage (due to their sponge-like and asymmetric  
357 structure to serve as a better reservoir for MPD) and the confinement effect (due to the  
358 tortuous pores and therefore greater resistance to degassed nanobubbles) (Figure 5C).  
359 Following these criteria, coating a microporous interlayer on a conventional substrate may  
360 be highly beneficial to further enhance MPD uptake<sup>19</sup> as well as the gas confinement effect.  
361 Indeed, several studies have demonstrated one order of magnitude improvement in  
362 membrane permeability by the simple incorporation of an interlayer.<sup>19,50</sup> The current study,  
363 in concert with other recent literature studies, reveals the huge potential for further  
364 optimization of TFC RO membranes as well as the critical need to conduct more systematic  
365 and mechanistic studies on the fundamental roles of membrane substrates.

366

367 The current study along with other recent membrane characterization works<sup>25, 29-34</sup> also  
368 provide important inputs to the development of more accurate simulation studies on the  
369 formation of polyamide RO membranes. For example, recent studies on multiscale  
370 molecular simulation predict an intrinsic film thickness on the order of 10 nm for  
371 polyamide formed by the IP reaction of MPD and TMC,<sup>51, 52</sup> which agrees reasonably well  
372 with electron microscopic characterization results.<sup>25, 32-34</sup> Nevertheless, the simulated  
373 surface roughness of 1 – 4 nm<sup>52</sup> was two orders of magnitude below the typical values for  
374 fully aromatic polyamide membranes.<sup>25, 33, 34, 53</sup> Future simulation studies should consider  
375 the inclusion of the interfacial degassing mechanism<sup>25, 35-38</sup> in order to provide more  
376 accurate predictions of surface roughness.

377

## 378 **SUPPORTING INFORMATION**

379 S1. Determination of pore density and porosity; S2 Properties of the backside openings of  
380 polyamide films; S3 Effect of hydrophilicity of substrates; S4 Theoretical calculations for  
381 CO<sub>2</sub> degassing; S5. Resolving the intrinsic permeability of TFC-PCTE membrane. This  
382 material is available free of charge via the Internet at <http://pubs.acs.org>.

383

## 384 **ACKNOWLEDGMENTS**

385 The work is partially supported by a grant from the Research Grants Council of the Hong  
386 Kong Special Administration Region, China (C7051-17G).

## REFERENCES

1. Lee, K. P.; Arnot, T. C.; Mattia, D., A review of reverse osmosis membrane materials for desalination—Development to date and future potential. *J. Membr. Sci.* **2011**, *370*, (1-2), 1-22.
2. Park, H. B.; Kamcev, J.; Robeson, L. M.; Elimelech, M.; Freeman, B. D., Maximizing the right stuff: The trade-off between membrane permeability and selectivity. *Science* **2017**, *356*, (6343), eaab0530.
3. Qasim, M.; Badrelzaman, M.; Darwish, N. N.; Darwish, N. A.; Hilal, N., Reverse osmosis desalination: A state-of-the-art review. *Desalination* **2019**, *459*, 59-104.
4. Yang, Z.; Guo, H.; Tang, C. Y. Y., The upper bound of thin-film composite (TFC) polyamide membranes for desalination. *J. Membr. Sci.* **2019**, *590*, 117297.
5. Greenlee, L. F.; Lawler, D. F.; Freeman, B. D.; Marrot, B.; Moulin, P., Reverse osmosis desalination: water sources, technology, and today's challenges. *Water Res.* **2009**, *43*, (9), 2317-48.
6. Xie, M.; Shon, H. K.; Gray, S. R.; Elimelech, M., Membrane-based processes for wastewater nutrient recovery: Technology, challenges, and future direction. *Water Res.* **2016**, *89*, 210-21.
7. Tang, C. Y.; Yang, Z.; Guo, H.; Wen, J. J.; Nghiem, L. D.; Cornelissen, E., Potable Water Reuse through Advanced Membrane Technology. *Environ. Sci. Technol.* **2018**, *52*, (18), 10215-10223.
8. Lin, S., Energy Efficiency of Desalination: Fundamental Insights from Intuitive Interpretation. *Environ. Sci. Technol.* **2020**, *54*, (1), 76-84.
9. Hirose, M.; Ito, H.; Kamiyama, Y., Effect of skin layer surface structures on the flux behaviour of RO membranes. *J. Membr. Sci.* **1996**, *121*, (2), 209-215.
10. Mulder, M., *Basic principles of membrane technology*. 2nd ed.; Kluwer Academic: Dordrecht; Boston, 1996; p 564 p.
11. Kim, S. H.; Kwak, S. Y.; Suzuki, T., Positron annihilation spectroscopic evidence to demonstrate the flux-enhancement mechanism in morphology-controlled thin-film-composite (TFC) membrane. *Environ. Sci. Technol.* **2005**, *39*, (6), 1764-1770.
12. Ghosh, A. K.; Hoek, E. M. V., Impacts of support membrane structure and chemistry on polyamide-polysulfone interfacial composite membranes. *J. Membr. Sci.* **2009**, *336*, (1-2), 140-148.
13. Huang, L.; McCutcheon, J. R., Impact of support layer pore size on performance of thin film composite membranes for forward osmosis. *J. Membr. Sci.* **2015**, *483*, 25-33.
14. Li, X. S.; Li, Q.; Fang, W. X.; Wang, R.; Krantz, W. B., Effects of the support on the characteristics and permselectivity of thin film composite membranes. *J. Membr. Sci.* **2019**, *580*, 12-23.
15. Singh, P. S.; Joshi, S. V.; Trivedi, J. J.; Devmurari, C. V.; Rao, A. P.; Ghosh, P. K., Probing the structural variations of thin film composite RO membranes obtained by coating polyamide over polysulfone membranes of different pore dimensions. *J. Membr. Sci.* **2006**, *278*, (1-2), 19-25.
16. Ramon, G. Z.; Wong, M. C. Y.; Hoek, E. M. V., Transport through composite membrane, part 1: Is there an optimal support membrane? *J. Membr. Sci.* **2012**, *415-416*, 298-305.
17. Wijmans, J. G.; Hao, P., Influence of the porous support on diffusion in composite membranes. *J. Membr. Sci.* **2015**, *494*, 78-85.
18. Park, S.-J.; Choi, W.; Nam, S.-E.; Hong, S.; Lee, J. S.; Lee, J.-H., Fabrication of polyamide thin film composite reverse osmosis membranes via support-free interfacial polymerization. *J. Membr. Sci.* **2017**, *526*, 52-59.



19. Yang, Z.; Zhou, Z. W.; Guo, H.; Yao, Z.; Ma, X. H.; Song, X.; Feng, S. P.; Tang, C. Y., Tannic Acid/Fe(3+) Nanoscaffold for Interfacial Polymerization: Toward Enhanced Nanofiltration Performance. *Environ. Sci. Technol.* **2018**, *52*, (16), 9341-9349.
20. Yan, H.; Miao, X.; Xu, J.; Pan, G.; Zhang, Y.; Shi, Y.; Guo, M.; Liu, Y., The porous structure of the fully-aromatic polyamide film in reverse osmosis membranes. *J. Membr. Sci.* **2015**, *475*, 504-510.
21. Ding, C.; Yin, J.; Deng, B., Effects of polysulfone (PSf) support layer on the performance of thin-film composite (TFC) membranes. *J. Chem. Proc. Eng.* **2014**, *1*, 1-8.
22. Wang, J.; Xu, R.; Yang, F.; Kang, J.; Cao, Y.; Xiang, M., Probing influences of support layer on the morphology of polyamide selective layer of thin film composite membrane. *J. Membr. Sci.* **2018**, *556*, 374-383.
23. Song, Y.; Sun, P.; Henry, L.; Sun, B., Mechanisms of structure and performance controlled thin film composite membrane formation via interfacial polymerization process. *J. Membr. Sci.* **2005**, *251*, (1-2), 67-79.
24. Ehsan Yakavangi, M.; Rimaz, S.; Vatanpour, V., Effect of surface properties of polysulfone support on the performance of thin film composite polyamide reverse osmosis membranes. *J. Appl. Polym. Sci.* **2016**, *134*, (6), 44444.
25. Song, X.; Gan, B.; Qi, S.; Guo, H.; Tang, C. Y.; Zhou, Y.; Gao, C., Intrinsic Nanoscale Structure of Thin Film Composite Polyamide Membranes: Connectivity, Defects, and Structure-Property Correlation. *Environ. Sci. Technol.* **2020**, *54*, (6), 3559-3569.
26. Elimelech, M.; Zhu, X. H.; Childress, A. E.; Hong, S. K., Role of membrane surface morphology in colloidal fouling of cellulose acetate and composite aromatic polyamide reverse osmosis membranes. *J. Membr. Sci.* **1997**, *127*, (1), 101-109.
27. Tang, C. Y. Y.; Kwon, Y. N.; Leckie, J. O., Probing the nano- and micro-scales of reverse osmosis membranes - A comprehensive characterization of physiochemical properties of uncoated and coated membranes by XPS, TEM, ATR-FTIR, and streaming potential measurements. *J. Membr. Sci.* **2007**, *287*, (1), 146-156.
28. Kong, C.; Kanezashi, M.; Yamamoto, T.; Shintani, T.; Tsuru, T., Controlled synthesis of high performance polyamide membrane with thin dense layer for water desalination. *J. Membr. Sci.* **2010**, *362*, (1-2), 76-80.
29. Pacheco, F. A.; Pinnau, I.; Reinhard, M.; Leckie, J. O., Characterization of isolated polyamide thin films of RO and NF membranes using novel TEM techniques. *J. Membr. Sci.* **2010**, *358*, (1-2), 51-59.
30. Pacheco, F.; Sougrat, R.; Reinhard, M.; Leckie, J. O.; Pinnau, I., 3D visualization of the internal nanostructure of polyamide thin films in RO membranes. *J. Membr. Sci.* **2016**, *501*, 33-44.
31. Lin, L.; Lopez, R.; Ramon, G. Z.; Coronell, O., Investigating the void structure of the polyamide active layers of thin-film composite membranes. *J. Membr. Sci.* **2016**, *497*, 365-376.
32. Karan, S.; Jiang, Z. W.; Livingston, A. G., Sub-10 nm polyamide nanofilms with ultrafast solvent transport for molecular separation. *Science* **2015**, *348*, (6241), 1347-1351.
33. Kłosowski, M. M.; McGilvery, C. M.; Li, Y.; Abellan, P.; Ramasse, Q.; Cabral, J. T.; Livingston, A. G.; Porter, A. E., Micro-to nano-scale characterisation of polyamide structures of the SW30HR RO membrane using advanced electron microscopy and stain tracers. *J. Membr. Sci.* **2016**, *520*, 465-476.
34. Song, X.; Smith, J. W.; Kim, J.; Zaluzec, N. J.; Chen, W.; An, H.; Dennison, J. M.; Cahill, D. G.; Kulzick, M. A.; Chen, Q., Unraveling the Morphology-Function Relationships of Polyamide Membranes Using Quantitative Electron Tomography. *ACS Appl Mater Interfaces* **2019**, *11*, (8), 8517-8526.

35. Ma, X.-H.; Yao, Z.-K.; Yang, Z.; Guo, H.; Xu, Z.-L.; Tang, C. Y.; Elimelech, M., Nanofoaming of Polyamide Desalination Membranes To Tune Permeability and Selectivity. *Environ. Sci. Technol. Lett.* **2018**, *5*, (2), 123-130.
36. Ma, X.; Yang, Z.; Yao, Z.; Guo, H.; Xu, Z.; Tang, C. Y., Tuning roughness features of thin film composite polyamide membranes for simultaneously enhanced permeability, selectivity and anti-fouling performance. *J. Colloid Interface Sci.* **2019**, *540*, 382-388.
37. Peng, L. E.; Yao, Z.; Liu, X.; Deng, B.; Guo, H.; Tang, C. Y., Tailoring Polyamide Rejection Layer with Aqueous Carbonate Chemistry for Enhanced Membrane Separation: Mechanistic Insights, Chemistry-Structure-Property Relationship, and Environmental Implications. *Environ. Sci. Technol.* **2019**, *53*, (16), 9764-9770.
38. Song, X.; Gan, B.; Yang, Z.; Tang, C. Y.; Gao, C., Confined nanobubbles shape the surface roughness structures of thin film composite polyamide desalination membranes. *J. Membr. Sci.* **2019**, *582*, 342-349.
39. Yao, Z.; Guo, H.; Yang, Z.; Qing, W.; Tang, C. Y., Preparation of nanocavity-contained thin film composite nanofiltration membranes with enhanced permeability and divalent to monovalent ion selectivity. *Desalination* **2018**, *445*, 115-122.
40. Jiang, Z.; Karan, S.; Livingston, A. G., Water Transport through Ultrathin Polyamide Nanofilms Used for Reverse Osmosis. *Adv. Mater.* **2018**, *30*, (15), 1705973.
41. Li, X.; Wang, K. Y.; Helmer, B.; Chung, T.-S., Thin-Film Composite Membranes and Formation Mechanism of Thin-Film Layers on Hydrophilic Cellulose Acetate Propionate Substrates for Forward Osmosis Processes. *Ind. Eng. Chem. Res.* **2012**, *51*, (30), 10039-10050.
42. Liu, B.; Chen, C.; Zhao, P.; Li, T.; Liu, C.; Wang, Q.; Chen, Y.; Crittenden, J., Thin-film composite forward osmosis membranes with substrate layer composed of polysulfone blended with PEG or polysulfone grafted PEG methyl ether methacrylate. *Frontiers Chem. Sci. Eng.* **2016**, *10*, (4), 562-574.
43. Xu, J.; Yan, H.; Zhang, Y.; Pan, G.; Liu, Y., The morphology of fully-aromatic polyamide separation layer and its relationship with separation performance of TFC membranes. *J. Membr. Sci.* **2017**, *541*, 174-188.
44. Jimenez-Solomon, M. F.; Gorgojo, P.; Munoz-Ibanez, M.; Livingston, A. G., Beneath the surface: Influence of supports on thin film composite membranes by interfacial polymerization for organic solvent nanofiltration. *J. Membr. Sci.* **2013**, *448*, 102-113.
45. Yao, Z.; Guo, H.; Yang, Z.; Lin, C.; Zhu, B.; Dong, Y.; Tang, C. Y., Reactable substrate participating interfacial polymerization for thin film composite membranes with enhanced salt rejection performance. *Desalination* **2018**, *436*, 1-7.
46. Yao, Z.; Yang, Z.; Guo, H.; Ma, X.; Dong, Y.; Tang, C. Y., Highly permeable and highly selective ultrathin film composite polyamide membranes reinforced by reactable polymer chains. *J. Colloid Interface Sci.* **2019**, *552*, 418-425.
47. She, Q.; Hou, D.; Liu, J.; Tan, K. H.; Tang, C. Y., Effect of feed spacer induced membrane deformation on the performance of pressure retarded osmosis (PRO): Implications for PRO process operation. *J. Membr. Sci.* **2013**, *445*, 170-182.
48. Lee, C.; Jang, J.; Tin, N. T.; Kim, S.; Tang, C. Y.; Kim, I. S., Effect of spacer configuration on the characteristics of FO membranes: Alteration of permeation characteristics by membrane deformation and concentration polarization. *Environ. Sci. Technol.* **2020**, in press (<https://doi.org/10.1021/acs.est.9b06921>).
49. Li, Y.; Kłosowski, M. M.; McGilvery, C. M.; Porter, A. E.; Livingston, A. G.; Cabral, J. T., Probing flow activity in polyamide layer of reverse osmosis membrane with nanoparticle tracers. *J. Membr. Sci.* **2017**, *534*, 9-17.

50. Zhou, Z.; Hu, Y.; Boo, C.; Liu, Z.; Li, J.; Deng, L.; An, X., High-Performance Thin-Film Composite Membrane with an Ultrathin Spray-Coated Carbon Nanotube Interlayer. *Environ. Sci. Technol. Lett.* **2018**, *5*, (5), 243-248.
51. Oizerovich-Honig, R.; Raim, V.; Srebniak, S., Simulation of Thin Film Membranes Formed by Interfacial Polymerization. *Langmuir* **2010**, *26*, (1), 299-306.
52. Muscatello, J.; Müller, E. A.; Mostofi, A. A.; Sutton, A. P., Multiscale molecular simulations of the formation and structure of polyamide membranes created by interfacial polymerization. *J. Membr. Sci.* **2017**, *527*, 180-190.
53. Tang, C. Y.; Kwon, Y.-N.; Leckie, J. O., Effect of membrane chemistry and coating layer on physiochemical properties of thin film composite polyamide RO and NF membranes II. Membrane physiochemical properties and their dependence on polyamide and coating layers. *Desalination* **2009**, *242*, (1-3), 168-182.