

# 1 Sulfate Radical-Induced Destruction of Emerging Contaminants Using Traces

## 2 of Cobalt Ions as Catalysts

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16 *Submitted to Chemosphere*

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## 26 WORD COUNTs:

## 27 Text about 4735 w

28 Acknowledgements) + 6 Figures = 6535 words

29 **ABSTRACT**

30 Cobalt is part of vitamin B12, which is essential to maintain human health, and trace levels of  
31 cobalt ions are ubiquitous in water and soil environments. In this study, the destruction of 1,4-  
32 dioxane (1,4-D) by peroxyomonosulfate (PMS) under the catalysis of trace levels of  $\text{Co}^{2+}$  was  
33 investigated under buffered conditions. The results showed that near 100% removal of 1,4-D  
34 was achieved after reaction for 6 and 10 min with 50 and 25  $\mu\text{g/L}$   $\text{Co}^{2+}$ , respectively, in the  
35 presence of 5 mM phosphate ions. Mechanism studies revealed that radicals mediated the  
36 destruction of 1,4-D and sulfate radicals were the primary reactive species. The traces of  $\text{Co}^{2+}$   
37 had the greatest reactivity for the catalysis of PMS in neutral environments (pH 7.0). However,  
38 pH 5.5 was observed to be the best condition for 1,4-D destruction, which was probably caused  
39 by the involvement of phosphate radicals. Common water components including chloride ions  
40 and bicarbonate ions were observed to have promoting and inhibiting effects, respectively, on  
41 the removal of 1,4-D. To further demonstrate the potential of  $\text{Co}^{2+}$ -PMS in practical  
42 applications, we explored the simultaneous degradation of 20 antibiotics using trace levels of  
43  $\text{Co}^{2+}$ . The results showed that all the investigated antibiotics, except for lomefloxacin, could  
44 be efficiently degraded by  $\text{Co}^{2+}$ -PMS with removal rates of greater than 97%. The findings  
45 from this study demonstrate the promise of using trace levels of cobalt for environmental  
46 remediation applications, even when high concentrations of phosphate ions are co-present.

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52 **Keywords:** 1,4-Dioxane; Antibiotics; Sulfate radicals; Degradation; Persulfate; Emerging  
53 contaminants

54 **1. Introduction**

55 1,4-Dioxane (1,4-D), a cyclic compound, is widely employed as an organic solvent in many  
56 industrial products. It is also commonly used to stabilize chlorinated solvents, particularly  
57 1,1,1-trichloroethane, and is generated as a by-product in a wide range of consumer products  
58 (Mohr et al., 2010; Milavec et al., 2019). Due to the improper treatment of industrial wastes  
59 and organic solvents, leakage of 1,4-D into the environment has been documented (Mohr et al.,  
60 2010). 1,4-D is resistant to microbial treatment and has a very low soil sorption partition  
61 coefficient, which renders itself highly mobile in environmental matrices (Adamson et al.,  
62 2015). 1,4-D is miscible in water and has a low octanol–water partition coefficient ( $K_{ow}$ ,  $10^{0.27}$ )  
63 and low vapor pressure (37 mmHg, 25 °C), which makes itself difficult to be removed by  
64 conventional physical purification technologies, such as adsorption and air stripping (Sekar  
65 and DiChristina, 2014). In addition, traditional oxidants having a standard reduction potential  
66 of lower than 2.0 V are generally considered ineffective for the treatment of 1,4-D (Eberle et  
67 al., 2016). Although this substance has been recognized as a drinking water contaminant since  
68 1978, a very recent study showed that the 1,4-D level in the drinking water of near 30 million  
69 people in the United States exceeds the health-based reference regulation (McElroy et al., 2019).

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71 1,4-D has been classified as a carcinogen (Class 2B) and listed as an emerging contaminant by  
72 the U.S. EPA (Patton et al., 2016). Advanced oxidation processes (AOPs), particularly those  
73 relying on strong oxidizing radicals, such as hydroxyl radicals ( $\cdot OH$ ,  $E^0 (\cdot OH/OH^-) = 1.8-2.7$   
74 V) and sulfate radicals ( $SO_4^{2-}$ ,  $E^0 (SO_4^{2-}/SO_4^{2-}) = 2.5-3.1$  V) (Buxton et al., 1988) (Neta et al.,  
75 1988), are compelling technologies for the treatment of recalcitrant contaminants and have  
76 been investigated to degrade 1,4-D. To generate  $\cdot OH$  for 1,4-D degradation, sonication (Son et  
77 al., 2006), Fenton reagents (Merayo et al., 2014), photocatalysis (Barndők et al., 2016), and  
78 UV-assisted Fenton-like reactions (Patton et al., 2018) have been studied. Although  $\cdot OH$  is

79 highly reactive toward 1,4-D  $[(1.1\text{-}2.4) \times 10^9 \text{ M}^{-1} \text{ s}^{-1}]$  (Adams et al., 1994), the application  
80 of  $\cdot\text{OH}$ -based AOPs in practical applications suffers from known scavenging problems due to  
81 the ubiquitous presence of radical scavengers (Hodges et al., 2018). Compared with  $\cdot\text{OH}$  ( $t_{1/2}$   
82  $= 10^{-3} \mu\text{s}$ ),  $\text{SO}_4^{\cdot-}$  is more selective and has a significantly longer lifetime ( $t_{1/2} = 30\text{-}40 \mu\text{s}$ ).  
83 However, the later reactive species is significantly less investigated for 1,4-D removal  
84 (Cashman et al., 2019). The generation of  $\text{SO}_4^{\cdot-}$  usually depends on the activation of either  
85 peroxydisulfate (PDS) or peroxymonosulfate (PMS) (Wang et al., 2014). Among the persulfate  
86 technologies reported for 1,4-D degradation, iron is the most commonly used material.  
87 Different forms of iron, such as  $\text{Fe}^{2+}$  (Zhao et al., 2014), zero-valent iron (Pang et al., 2019),  
88 iron oxides (Zhong et al., 2015), and iron minerals (Feng et al., 2018a), have been tested.  
89 Although decent performance was achieved, iron does not demonstrate true catalytic activity  
90 in these studies; the regeneration of ferrous iron is thermodynamically unfavourable and iron  
91 sludge is accumulated after neutralization (Hou et al., 2017).



94  
95 Since its first-time application in pollutant removal (Anipsitakis and Dionysiou, 2003), the  
96 combination of PMS with  $\text{Co}^{2+}$  has been known for its powerful oxidizing capability. A similar  
97 performance could be achieved between the combinations of  $\text{Co}^{2+}$ -PMS and  $\text{Fe}^{2+}$ - $\text{H}_2\text{O}_2$  even if  
98 the concentration of  $\text{Co}^{2+}$  is 100 times lower than that of the  $\text{Fe}^{2+}$  (Bandala et al., 2007). This  
99 is not only because of the efficient activation of PMS by  $\text{Co}^{2+}$  to generate  $\text{SO}_4^{\cdot-}$  (Eq. 1), but also  
100 because of the thermodynamic feasible reduction of  $\text{Co}^{3+}$  [ $E^0(\text{Co}^{3+}/\text{Co}^{2+}) = 1.92 \text{ V}$ ] by PMS  
101 (Eq. 2) [ $E^0(\text{HSO}_5^-/\text{SO}_4^{2-}) = 1.75 \text{ V}$ ] (Anipsitakis and Dionysiou, 2004). In addition, aqueous  
102  $\text{Co}^{2+}$  ions are stable under aerobic conditions; the oxidation of  $\text{Co}^{2+}$  by dissolved molecular  
103 oxygen is extremely slow ( $10^{-20.8} \text{ M}^{-1} \text{ s}^{-1}$ ) (Rosso and Morgan, 2002). Although  $\text{Co}^{2+}$  can serve

104 as a real catalyst, its remanence in water solutions after treatment is a concern because of the  
105 potential toxicity of elevated levels of cobalt ions, which greatly limits its practical application.  
106 To this end, various solid Co-containing activators, such as cobalt oxides (Pang et al., 2020),  
107 cobalt bimetallic oxides (Ren et al., 2015), and Co-doped carbonaceous materials (Li et al.,  
108 2016), have been prepared and tested for PMS activation. However, trace levels of cobalt ions  
109 are still leached out even from stable Co-doped carbonaceous materials. For example, around  
110 230  $\mu\text{g/L}$  of cobalt ions were leached out from a highly efficient cobalt-graphene material (Li  
111 et al., 2018b). As the leaching seems inevitable, the purpose of this study was to examine the  
112 oxidative capability of PMS under the catalysis of trace levels of  $\text{Co}^{2+}$  ( $\leq 50 \mu\text{g/L}$ ) with 1,4-D  
113 and antibiotics as the target emerging contaminants. Antibiotics are widely used and frequently  
114 detected in the environments (Zhang et al., 2015), which is a great health concern. The  
115 concentration of  $\text{Co}^{2+}$  investigated in this study is lower than the level of  $\text{Co}^{2+}$  (usually greater  
116 than 100  $\mu\text{g/L}$ ) used to homogeneously catalyse PMS in literatures (Chen et al., 2019) and is  
117 comparable with the actual cobalt concentrations in various environmental matrices,  
118 particularly in soils and sediments (Collins and Kinsela, 2010; Izah et al., 2016).  
119

120 **2. Experimental section**

121 **2.1 Chemicals**

123 PMS (Oxone ( $2\text{KHSO}_5 \cdot \text{KHSO}_4 \cdot \text{K}_2\text{SO}_4$ ))), anhydrous 1,4-D (99.8%), sodium bicarbonate (99.5-  
124 100.5%), sodium thiosulfate ( $\geq 99\%$ ), nitrobenzene (99%), and sodium chloride ( $\geq 99.8\%$ )  
125 were supplied by Sigma-Aldrich (St. Louis, MO, USA). *tert*-Butanol (99.5%) and 2,4-  
126 dinitrophenylhydrazine (98%) were obtained from Aladdin Corp. (Shanghai, China).  
127 Potassium iodide (99.8%) and sulfuric acid (98%) were purchased from BDH Chemicals  
128 (Poole, UK). Cobalt(II) nitrate hexahydrate (99%) and liquid chromatography (LC)-mass  
129 spectrometry (MS)-grade acetonitrile (methanol) were obtained from Merck Corp. (Darmstadt,

130 Germany). Twenty antibiotics with high purity (Table S1) were supplied by Dr. Ehrenstorfer  
131 GmbH (Germany).

132

133 2.2 Catalytic and degradation experiments

134 All the catalytic destruction reactions were conducted in 200-mL glass reactors at ambient  
135 temperature ( $25 \pm 1$  °C). The stock solutions of PMS (0.5 M),  $\text{Co}^{2+}$  (0.1 M), and 1,4-D (10 g/L)  
136 were prepared in advance by dissolving desired doses of Oxone,  $\text{Co}(\text{NO}_3)_2$  powders, and  
137 anhydrous 1,4-D, respectively, in ultrapure water. Typically, ultrapure water (100 mL) was  
138 transferred to the reactor, followed by the addition of 1,4-D, PMS, and phosphate buffer. The  
139 pH value of the resulting solution was adjusted when necessary using diluted NaOH and  $\text{H}_2\text{SO}_4$   
140 solutions. To initiate catalytic and destruction reactions,  $\text{Co}^{2+}$  ( $\text{Co}(\text{NO}_3)_2$  solution) was then  
141 added to the system. Liquid samples (1 mL) were collected using a pipette, transferred to LC  
142 auto-sampler vials (2 mL), and quenched immediately using excess sodium thiosulfate. The  
143 resulting samples were analysed within 30 min.

144

145 During the study of antibiotics, a stock solution containing 20 antibiotics (2 mg/L for each  
146 antibiotic) was prepared by dissolving desired amounts of chemical powders in LC-MS-grade  
147 methanol. To investigate their degradation by  $\text{Co}^{2+}$ -PMS, the antibiotic stock solution was then  
148 dried under nitrogen flow and redissolved in ultrapure water to achieve a target concentration  
149 of 50  $\mu\text{g/L}$  for each compound. Before the analysis, the samples withdrawn were diluted with  
150 LC-MS-grade methanol and ultrapure water for 50 times (the diluted samples contained 50%  
151 of methanol (v/v)). Other steps were the same as that for the catalytic removal of 1,4-D.

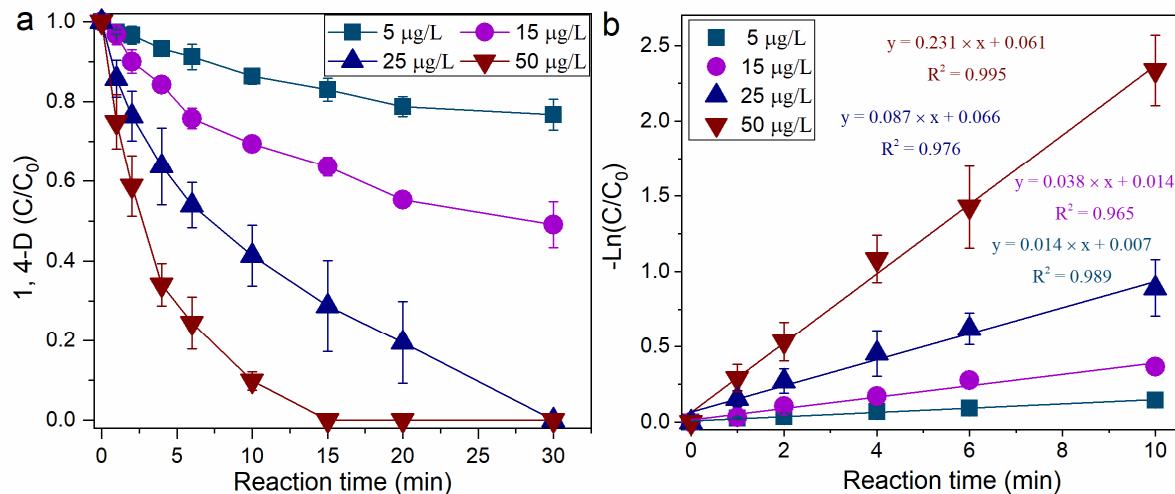
152

153 2.3 Analysis of chemicals

154 1,4-D was measured using an Agilent 1260 Infinity II high-performance LC (HPLC) system  
155 equipped with a diode array detector (DAD) and an auto-sampler. A ZORBAX Eclipse XDB-  
156 C18 column (4.6 × 150 mm, 5  $\mu$ m) was used for the separation. HPLC-grade acetonitrile and  
157 ultrapure water (10:90, v/v) were used as the mobile phase with a flow rate of 1 mL/min at a  
158 column temperature of 30 °C. The DAD wavelength was set at 190 nm. The retention time of  
159 1,4-D was around 2.4 min and the detection limit of 1,4-D was lower than 0.2 mg/L. PMS was  
160 quantified spectrometrically using an iodometric approach (Liang et al., 2008). The total  
161 organic carbon (TOC) was quantified using a TOC analyser (Shimadzu TOC-L series) via the  
162 combustion catalytic oxidation approach. Formaldehyde (HCHO) was quantified after reaction  
163 with 2,4-dinitrophenylhydrazine, details of which can be found in our previous publication  
164 (Feng et al., 2017a).

165

166 Twenty antibiotics were measured using an Acquity ultra-performance LC (UPLC) I-Class  
167 system coupled to a Xevo TQ-S triple quadrupole mass spectrometer (Waters Corp. Milford,  
168 MA, USA) with electrospray ionization under a positive ionization mode (UPLC-(ESI<sup>+</sup>)-  
169 MS/MS). The separation was conducted on an Acquity UPLC BEH C18 column (2.1 mm × 50  
170 mm, 1.7  $\mu$ m). The quantification was carried out in multiple-reaction monitoring (MRM)  
171 modes. Detailed MRM transitions and the retention time of antibiotics are listed in Table S1.  
172 The injection volume of each sample was 2  $\mu$ L, and the column temperature was fixed at 40 °C.  
173 The mobile phases consisted of ultrapure water (0.1% (v/v) formic acid, A) and methanol (B).  
174 The gradient program of the mobile phase is listed in Table S2. Details of MS parameters  
175 include a source temperature of 150 °C, a desolvation temperature of 500 °C, desolvation gas  
176 flow of 1,000 L/h, and cone gas flow of 150 L/h. The quantification of limit for each antibiotic  
177 was lower than 20 ng/L, and calibration curves were established with a series of concentrations  
178 in the range of 20 to 1,000 ng/L.

179 **3. Results and discussion**180 **3.1 Catalytic destruction of 1,4-D**

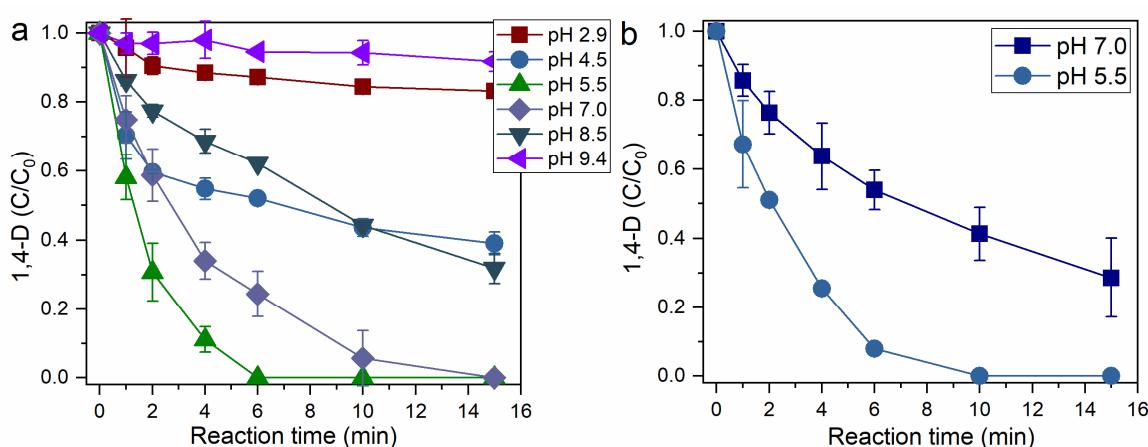
181  
182 **Figure 1. (a) Destruction of 1,4-D by PMS under the catalysis of different levels of  $\text{Co}^{2+}$  and**  
183 **(b) the corresponding pseudo-first-order rate constants (slopes). Experimental conditions:**  
184 **[PMS] = 2 mM, [1,4-D] = 5 mg/L, and 5 mM phosphate buffer at pH 7.0.**

185  
186 PMS alone had no obvious capability to degrade 1,4-D (Feng et al., 2017a). The destruction of  
187 1,4-D in  $\text{Co}^{2+}$ -PMS oxidation was investigated in the presence of different doses of  $\text{Co}^{2+}$ . As  
188 shown in Fig. 1a, near 100% destruction of 1,4-D was achieved after reaction for 15 min with  
189 50  $\mu\text{g}/\text{L}$   $\text{Co}^{2+}$  and 2 mM PMS. When the concentration of  $\text{Co}^{2+}$  was reduced to 25  $\mu\text{g}/\text{L}$ , similar  
190 destruction performance was observed after reaction for 30 min. These phenomena suggest that  
191 trace levels of  $\text{Co}^{2+}$  have great reactivity for 1,4-D destruction via the catalysis of PMS. The  
192 destruction of 1,4-D by  $\text{Co}^{2+}$ -PMS was well modelled by the pseudo-first-order law (Fig. 1b).  
193 By plotting  $-\ln(\text{C}/\text{C}_0)$  versus reaction time (min), the pseudo-first-order rate constants with 5,  
194 15, 25 and 50  $\mu\text{g}/\text{L}$  of  $\text{Co}^{2+}$  were calculated to be 0.014, 0.038, 0.087, and 0.231  $\text{min}^{-1}$  (Fig.  
195 1b), respectively.

196

197

198

199 3.2 Effect of pH on  $\text{Co}^{2+}$ -PMS  
200

201  
202 **Figure 2.** (a) Reactivity of  $\text{Co}^{2+}$ -PMS under different pH values and (b) destruction of 1,4-D  
203 by PMS under the catalysis of  $25 \mu\text{g/L}$   $\text{Co}^{2+}$ . Experimental conditions:  $[\text{PMS}] = 2 \text{ mM}$ ,  $[\text{Co}^{2+}]$   
204 = (a)  $50 \mu\text{g/L}$  and (b)  $25 \mu\text{g/L}$ ,  $[1,4\text{-D}] = 5 \text{ mg/L}$ ,  $5 \text{ mM}$  acetate buffer (pH 4.5),  $5 \text{ mM}$  phosphate  
205 buffer (pH 5.5, 7.0, 8.5), and  $5 \text{ mM}$  boric buffer (pH 9.4).

206  
207 Solution pH value is a key parameter in environmental redox chemistry. To fully demonstrate  
208 the oxidative capability of  $\text{Co}^{2+}$ -PMS, we studied the destruction of 1,4-D under different pH  
209 values. The results showed that both strongly acidic and alkaline environments were  
210 detrimental to the destruction; overall removal rates of only around 13% and 9% were achieved  
211 at the pH value of 2.9 and 9.4, respectively (Fig. 2a). The combination of  $\text{Co}^{2+}$  with PMS had  
212 the best reactivity at pH 5.5; near 100% destruction of 1,4-D was observed after reaction for  
213 only 6 min under the catalysis of  $50 \mu\text{g/L}$   $\text{Co}^{2+}$ . When  $25 \mu\text{g/L}$   $\text{Co}^{2+}$  was used, the reaction time  
214 for completely removing 1,4-D at pH 5.5 was extended to 10 min (Fig. 2b). To reveal the  
215 mineralization of 1,4-D, the removal of TOC was studied. The results demonstrated that only  
216 around 14.5% of the TOC was removed after reaction for 15 min (Fig. S2). This removal rate  
217 was significantly lower than the destruction rate of 1,4-D.

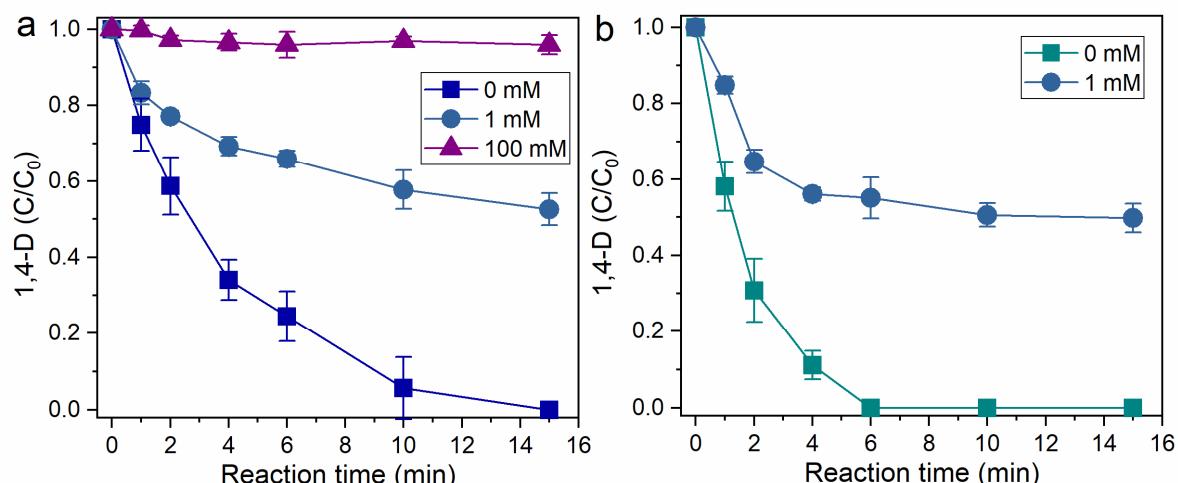
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219 The  $\text{p}K_{a,2}$  of PMS is around 9.4, and thus PMS primarily existed as  $\text{HSO}_5^-$  when the pH value  
220 ranged from 2.9 to 8.5. 1,4-D has a  $\text{p}K_a$  value of -2.92 (Perrin, 1972), which means that 1,4-D

221 existed as neutral molecules under the investigated pH conditions. The low reactivity at pH 2.9  
 222 could be related to the stabilization effect of excess  $\text{H}^+$  ions on the decomposition of PMS  
 223 (Zhang et al., 2013). In the pH range of 5.5 to 8.5, the degradation obviously slowed down,  
 224 which was probably caused by the variation in the speciation of cobalt ions.

225

226 3.3 Degradation mechanism and active species



227  
 228 **Figure 3. Influence of methanol on the destruction of 1,4-D in  $\text{Co}^{2+}$ -PMS oxidation at pH (a)**  
 229 **(b) 7.0 and (b) 5.5. Experimental conditions:  $[\text{PMS}] = 2 \text{ mM}$ ,  $[\text{Co}^{2+}] = 50 \mu\text{g/L}$ ,  $[1,4\text{-D}] = 5 \text{ mg/L}$ ,**  
 230 **and 5 mM phosphate buffer.**

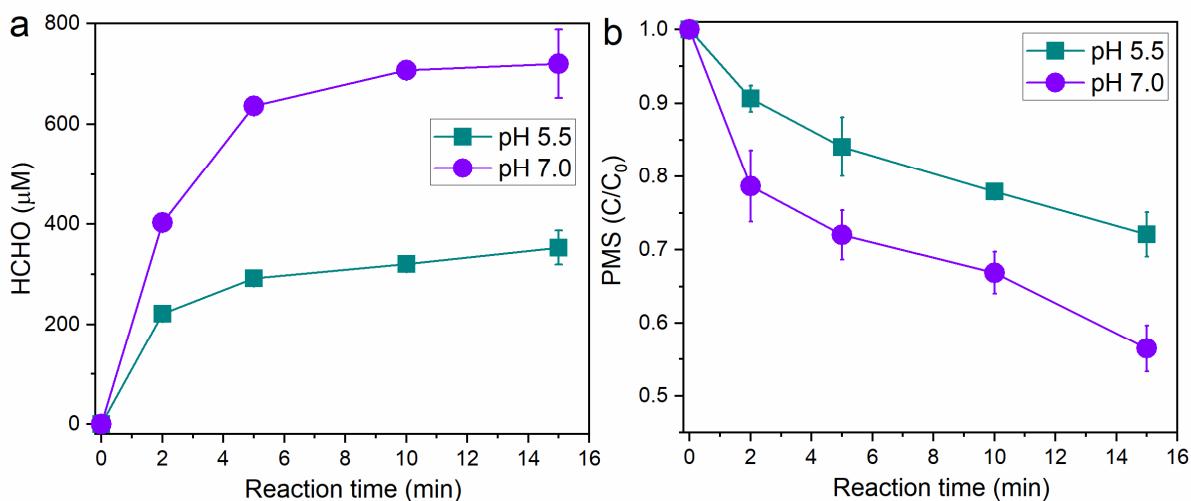
231  
 232 To examine the removal mechanism, the role of radicals in the degradation was investigated  
 233 by conducting scavenging experiments. Methanol reacts rapidly with both  $\text{SO}_4^{\cdot-}$  ( $2.5 \pm 0.4 \times$   
 234  $10^7 \text{ M}^{-1} \text{ s}^{-1}$ ) (Ross and Neta, 1979) and  $\cdot\text{OH}$  ( $9.7 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ ) (Buxton et al., 1988), and thus  
 235 this compound was used as a scavenger. The results revealed that the overall destruction rate  
 236 of 1,4-D decreased from around 100% to 47% and 50% at pH 7.0 (Fig. 3a) and pH 5.5 (Fig.  
 237 3b), respectively, in the presence of 1 mM methanol. When methanol was further increased to  
 238 100 mM, near complete inhibition of the degradation was observed (Fig. 3a). In addition to  
 239 radicals, singlet oxygen ( ${}^1\text{O}_2$ ) (Zhou et al., 2015), superoxide radicals ( $\text{O}_2^{\cdot-}$ ), and  
 240 peroxymonosulfate radical ( $\text{SO}_5^{\cdot-}$ ) were proposed to be generated as reactive species during the

241 activated decomposition of PMS. However,  $^1\text{O}_2$ -mediated oxidation cannot be quenched by  
242 methanol (Zhou et al., 2015), and therefore, the involvement of  $^1\text{O}_2$  can be excluded.  
243 Meanwhile, the contribution of  $\text{O}_2^-$  ( $E^0(\text{O}_2^-/\text{O}_2) = -0.33$  V) (Wardman, 1989) and  $\text{SO}_5^-$   
244 ( $E^0(\text{SO}_5^-/\text{HSO}_5^-) = 1.1$  V) (Neta et al., 1988) to the degradation of organic contaminants in  
245 homogeneous systems is usually negligible due to their low oxidation potential and rapid  
246 transformation (Qin et al., 2018). Therefore, it can be concluded that radicals ( $\text{SO}_4^-$ ,  $\cdot\text{OH}$ ) were  
247 key to the destruction of 1,4-D, which confirms the findings by Cashman et al. (Cashman et al.,  
248 2019).

249

250 *tert*-Butanol, without an  $\alpha$ -hydrogen in its structure, is usually the alcohol used to reveal the  
251 contribution of  $\text{SO}_4^-$ . However, our experiments showed that *tert*-butanol had significant  
252 interference in the analysis of 1,4-D, and therefore, nitrobenzene was instead used to further  
253 differentiate the produced radicals. In our previous work, nitrobenzene has shown effectiveness  
254 in the differentiation of  $\text{SO}_4^-$  and  $\cdot\text{OH}$  (Feng et al., 2017b); nitrobenzene can be rapidly  
255 oxidized by  $\cdot\text{OH}$  ( $3.9 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$ ), but is not very reactive toward  $\text{SO}_4^- (< 10^6 \text{ M}^{-1} \text{ s}^{-1})$  (Neta  
256 et al., 1977; Buxton et al., 1988). When  $\text{Co}^{2+}$  was absent, only 3.2% of the nitrobenzene was  
257 removed by PMS alone (Fig. S1). When 50  $\mu\text{g/L}$  of  $\text{Co}^{2+}$  is co-present with PMS, 27.1% of the  
258 nitrobenzene (0.1 mM) was degraded (Fig. S1). Under identical conditions, near 100% of the  
259 1,4-D (5.68  $\mu\text{M}$ ) was removed by  $\text{Co}^{2+}$ -PMS (Fig. 3a). For the oxidation of 1,4-D and  
260 nitrobenzene by radicals,  $\text{SO}_4^-$  has a relatively greater rate constant with 1,4-D [ $(4.1-5.7) \times 10^7$   
261  $\text{M}^{-1} \text{ s}^{-1}$ ] (Huie et al., 1991) and  $\cdot\text{OH}$  is relatively more reactive toward nitrobenzene ( $3.9 \times 10^9$   
262  $\text{M}^{-1} \text{ s}^{-1}$ ) (Buxton et al., 1988). Therefore, the greater degradation of 1,4-D than nitrobenzene  
263 reveals that  $\text{SO}_4^-$  was the dominant radicals produced in  $\text{Co}^{2+}$ -PMS oxidation, which is in line  
264 with Anipsitakis and Dionysiou's results (Anipsitakis and Dionysiou, 2003). However, the

265 obvious degradation of nitrobenzene by  $\text{Co}^{2+}$ -PMS suggests that  $\cdot\text{OH}$  was also involved, which  
 266 was probably due to the interaction of  $\text{SO}_4^{\cdot-}$  with  $\text{OH}^-$ . Meanwhile, the overall removal  
 267 percentage of TOC was less than 15% (Fig. S2), which can be explained by the dominance of  
 268  $\text{SO}_4^{\cdot-}$ . Small-molecular carboxylic acids and esters were the major products of 1,4-D oxidation  
 269 by  $\text{SO}_4^{\cdot-}$  and  $\cdot\text{OH}$  (Feng et al., 2017a), and in our previous work we have demonstrated that the  
 270 degradation of ethers, such as ethylene glycol diformate, is much more difficult than that of  
 271 1,4-D in  $\text{SO}_4^{\cdot-}$ -mediated oxidation (Feng et al., 2017a). In addition,  $\text{SO}_4^{\cdot-}$  is also relatively low  
 272 reactive toward common carboxylic acids, such as acetic acid ( $4.3 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$ ) (Huie and  
 273 Clifton, 1990).



274  
 275 **Figure 4.** (a) Generation of HCHO from methanol oxidation by  $\text{Co}^{2+}$ -PMS under different pH  
 276 values and (b) the corresponding decomposition of PMS. Conditions:  $[\text{PMS}] = 2 \text{ mM}$ ,  $[\text{Co}^{2+}]$   
 277 = 50  $\mu\text{g/L}$ ,  $[\text{methanol}] = 0.25 \text{ M}$ , and 5 mM phosphate buffer.

278  
 279 To further examine the catalysis of PMS by  $\text{Co}^{2+}$ , we quantified the produced reactive species  
 280 using excess methanol as a substrate. Under the attack of radicals, methanol is oxidized to  
 281 HCHO (Feng et al., 2017a). The results showed that HCHO was generated at both pH values,  
 282 but the overall HCHO produced at pH 7.0 (720.1  $\mu\text{M}$ ) was much greater than that produced at  
 283 pH 5.5 (349.5  $\mu\text{M}$ , Fig. 4). Correspondingly, more rapid decomposition of PMS occurred at  
 284 pH 7.0. According to Eq. 3, the stoichiometric efficiencies at pH 7.0 and 5.5 were calculated

285 to be around 83% and 63%, respectively. The generation of one mole of  $\text{SO}_4^{\cdot-}$  and regeneration  
286 of  $\text{Co}^{2+}$  requires two moles of PMS (Eqs. 1 and 2), the high stoichiometric efficiencies recorded  
287 in this study probably suggest the involvement of other species, such as  $\text{CH}_2\text{OH}\cdot$ , in the  
288 reduction of  $\text{Co}^{3+}$ . In addition, high-valent metal complexes are proposed to be generated as  
289 one of the oxidizing species during the interaction of some transition metals with PMS (Feng  
290 et al., 2018b; Li et al., 2018a), and thus the possible formation of  $\text{Co}^{\text{IV}}=\text{O}$  in  $\text{Co}^{2+}$ -PMS  
291 oxidation needs to be explored in future studies (Brunschwig et al., 1983; Pfaff et al., 2011).

292 Stoichiometric efficiency =  $\frac{\Delta[\text{HCHO}]}{\Delta[\text{PMS}]}$  (3)

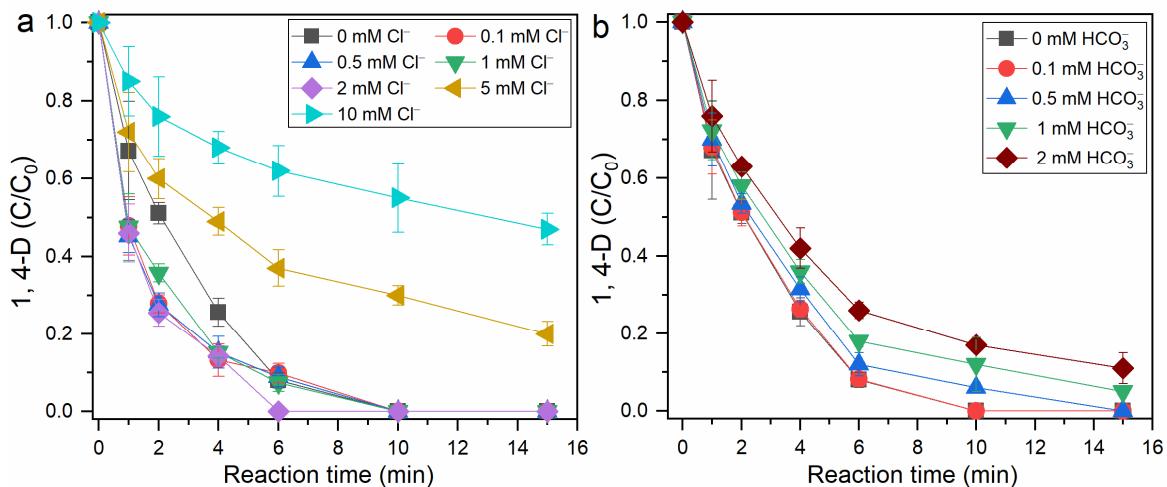
293  
294 The much greater generation of HCHO at pH 7.0 seems contrary with the destruction of 1,4-  
295 D observed in Fig. 2. As a relatively high level of phosphate buffer (5 mM, [phosphate  
296 buffer]/[1,4-D] = 88) was present, this discrepancy probably resulted from the scavenging  
297 effect of phosphate ions. The second-order rate constant between  $\text{SO}_4^{\cdot-}$  and  $\text{HPO}_4^{2-}$  is  $(1.2 \pm$   
298  $0.3) \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$ , and the rate constant of  $\text{SO}_4^{\cdot-}$  with 1,4-D is  $(4.1\text{-}5.7) \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ . Under  
299 the attack of  $\text{SO}_4^{\cdot-}$ , phosphate ions were transferred to phosphate radicals. According to the fast  
300 acid-base equilibria shown in Eq. 4 (Cencione et al., 1998), the primary phosphate radicals at  
301 pH 5.5 and pH 7.0 were  $\text{H}_2\text{PO}_4^{\cdot}$  and  $\text{HPO}_4^{\cdot}$ , respectively. The destruction of 1,4-D by  $\text{SO}_4^{\cdot-}$   
302 mainly proceeded via hydrogen abstraction (Huie et al., 1991).  $\text{H}_2\text{PO}_4^{\cdot}$  may have similar  
303 abstraction reactivity to  $\text{SO}_4^{\cdot-}$ , but the reactivity of  $\text{HPO}_4^{\cdot}$  and  $\text{PO}_4^{2-}$  are much weaker  
304 (Maruthamuthu and Neta, 1978). For example, the rate constants for the oxidation of  $\alpha$ ,  $\alpha$ ,  $\alpha$ -  
305 trifluorotoluene by  $\text{SO}_4^{\cdot-}$ ,  $\text{H}_2\text{PO}_4^{\cdot}$ ,  $\text{HPO}_4^{\cdot}$ , and  $\text{PO}_4^{2-}$  were  $(2 \pm 1) \times 10^7$ ,  $(3.5 \pm 0.5) \times 10^7$ ,  $(2.7$   
306  $\pm 0.5) \times 10^6$ , and  $(9 \pm 1) \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$  (Rosso et al., 1999), respectively. When the pH value  
307 rose from 5.5 to 7.0, the produced primarily phosphate radicals shifted from  $\text{H}_2\text{PO}_4^{\cdot}$  to  $\text{HPO}_4^{\cdot}$ ,  
308 which led to a decrease in the reactivity of the reaction system. However, the generation of  
309 phosphate radicals could be ignored when a high level of methanol (0.25 M) was present.

310 Therefore, it can be concluded that the combination of  $\text{Co}^{2+}$  with PMS had the greatest  
 311 reactivity at pH 7.0.



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314 3.4 Effects of chloride and bicarbonate ions



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 316 **Figure 5. Effects of (a)  $\text{Cl}^-$  and (b)  $\text{HCO}_3^-$  on the destruction of 1,4-D in  $\text{Co}^{2+}$ -PMS oxidation.**  
 317 Experimental conditions:  $[\text{PMS}] = 2 \text{ mM}$ ,  $[\text{Co}^{2+}] = 25 \mu\text{g/L}$ ,  $[1,4\text{-D}] = 5 \text{ mg/L}$ , and 5 mM  
 318 phosphate buffer (pH 5.5). The pH value of the 1,4-D solutions that contain phosphate buffer  
 319 (5 mM), varied levels of bicarbonate, and PMS was adjusted to 5.5 before the spiking of  $\text{Co}^{2+}$   
 320 to initiate catalytic degradation.

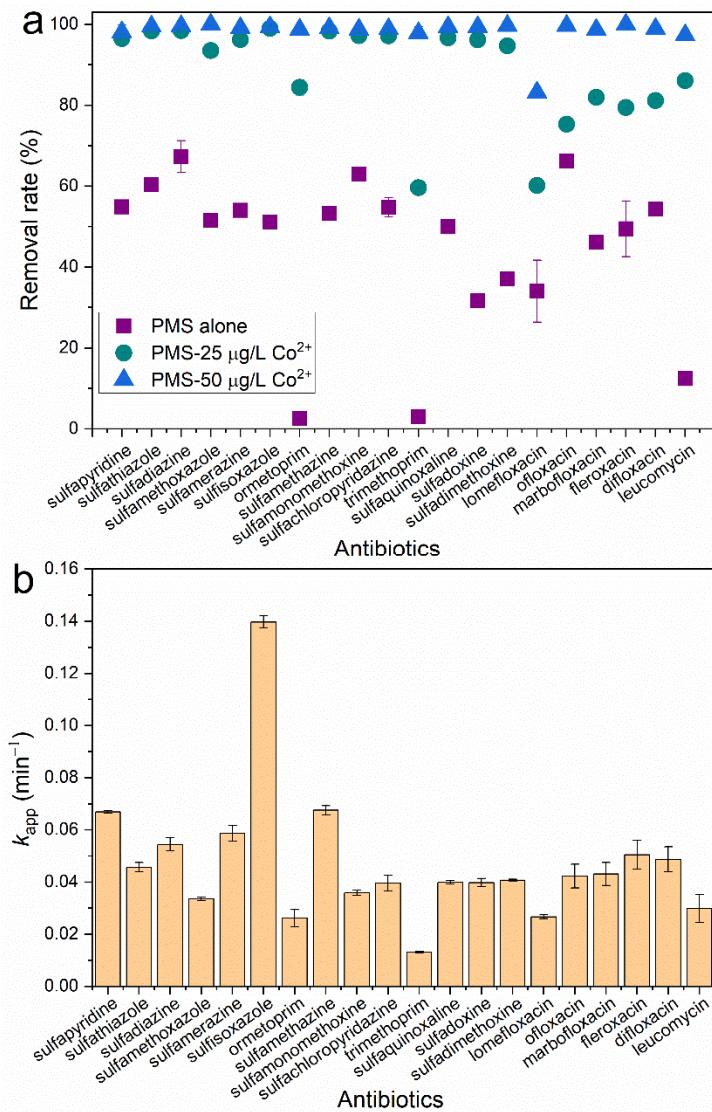
321  
 322 Chloride ions ( $\text{Cl}^-$ ) are ubiquitous in various water bodies and are common scavengers for  
 323 radicals, particularly for  $\text{SO}_4^{\cdot-}$ . Excess  $\text{Cl}^-$  ions react rapidly with  $\text{SO}_4^{\cdot-}$  ( $3.1 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$ ) to  
 324 generate chloride radicals [ $\text{Cl}_2^{\cdot-}, E^0(\text{Cl}_2^{\cdot-}/2\text{Cl}^-) = 2.09 \text{ V}$ ] and  $\text{Cl}_2^{\cdot-}$  is less reactive than  $\text{SO}_4^{\cdot-}$   
 325 [ $E^0(\text{SO}_4^{\cdot-}/\text{SO}_4^{2-}) = (2.5 - 3.1) \text{ V}$ ]. In previous publications, both promoting and inhibition  
 326 effects of  $\text{Cl}^-$  on  $\text{SO}_4^{\cdot-}$ -mediated oxidation have been reported (Chan and Chu, 2009; Feng et  
 327 al., 2018c). To demonstrate the capability of  $\text{Co}^{2+}$ -PMS for practical applications, the influence  
 328 of  $\text{Cl}^-$  on the destruction of 1,4-D was studied. The results showed that  $\text{Cl}^-$  with concentrations  
 329 in the range of 0.1 to 2 mM had no inhibitory effect on the degradation (Fig. 5a). Instead, a  
 330 slight promoting effect, particularly in the presence of 2 mM  $\text{Cl}^-$ , was observed. As discussed

331 above,  $\text{H}_2\text{PO}_4^-$  probably contributed to the degradation. The slight promoting effect possibly  
332 resulted from the reduced generation of  $\text{H}_2\text{PO}_4^-$  and the involvement of  $\text{Cl}_2^-$ . When the  
333 concentration of  $\text{Cl}^-$  was further increased to 5 and 10 mM, significant inhibitory effects were  
334 observed, which is consistent with our previous studies (Feng et al., 2017a; Feng et al., 2018a).  
335 Although the active chlorine species (e.g.,  $\text{Cl}_2^-$  and  $\text{HClO}$ ) generated in the presence of chloride  
336 ions are capable of oxidizing some organic contaminants and may even show promoting effects  
337 (Yuan et al., 2011; Huang et al., 2017; Sheng et al., 2018; Yang et al., 2018), these species are  
338 more selective than  $\text{SO}_4^{2-}$  and are relatively low reactive toward 1,4-D.  $\text{Cl}_2^-$  oxidizes 1,4-D at a  
339 second-order rate constant of  $(3.3 \pm 0.18) \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$  (Patton et al., 2016), and this value is  
340 significantly lower than the constant between  $\text{SO}_4^{2-}$  and 1,4-D  $[(4.1-5.7) \times 10^7 \text{ M}^{-1} \text{ s}^{-1}]$ .

341

342 In addition to  $\text{Cl}^-$ ,  $\text{HCO}_3^-$  ions are usually expected to consume radicals significantly in natural  
343 water. Meanwhile,  $\text{HCO}_3^-$  reacts with  $\text{SO}_4^{2-}$   $[(4.6 \pm 0.5) \times 10^6 \text{ M}^{-1} \text{ s}^{-1}]$  (Shafirovich et al., 2001)  
344 to generate less oxidizing carbonate radicals ( $\text{CO}_3^{2-}$ ,  $E^0 = (\text{CO}_3^{2-}/\text{CO}_3^{2-}) = 1.57 \text{ V}$ ) (Armstrong  
345 et al., 2013). Therefore, the influence of  $\text{HCO}_3^-$  on the destruction of 1,4-D was also studied.  
346 Results demonstrated that, in contrast to the promoting effect, the addition of  $\text{HCO}_3^-$  inhibited  
347 the destruction of 1,4-D (Fig. 5b). When  $\text{HCO}_3^-$  was in the range of 0.1 to 2 mM, the inhibitory  
348 extent was positively correlated with the concentration of  $\text{HCO}_3^-$ . These obvious scavenging  
349 effects could be explained by the consumption of  $\text{SO}_4^{2-}$  and the much weaker oxidative  
350 capability of  $\text{CO}_3^{2-}$ . The levels of  $\text{Cl}^-$  and  $\text{HCO}_3^-$  studied in this study are compatible with their  
351 contents in groundwater and surface water (Yang et al., 2015).

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Figure 6. (a) Simultaneous removal of 20 antibiotics by  $\text{Co}^{2+}$ -PMS and (b) their corresponding pseudo-first-order rate constants. Experimental conditions:  $[\text{PMS}] = 1 \text{ mM}$ , [each antibiotic] =  $50 \mu\text{g/L}$ , and reaction time = (a) 60 min and (b) 30 min. The initial pH value of the solution containing 20 antibiotics was not adjusted after the addition of PMS.

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One characteristic with the pollution of antibiotics is their relatively low concentrations and coexistence of various categories with different properties. To further demonstrate the practical applicability, we investigated the simultaneous degradation of 20 antibiotics by  $\text{Co}^{2+}$ -PMS. The antibiotics investigated here are widely used in China (Zhang et al., 2015). The results showed that most of the antibiotics could be degraded by unactivated PMS, although the removal rates (35 to 70%, Fig. 6a) are not satisfying. Antibiotics including ormetoprim, trimethoprim, and

365 leucomycin were relatively more resistant to PMS oxidation. When  $\text{Co}^{2+}$  ions were added as  
366 catalysts, the degradation of all the investigated antibiotics was significantly increased. The  
367 overall degradation rates of ormetoprim, trimethoprim, and leucomycin were increased from  
368 2.5%, 3.1%, and 12.4% to 84.4%, 59.7%, and 86.0%, respectively, in the presence of 25  $\mu\text{g/L}$   
369  $\text{Co}^{2+}$ . The degradation rates of all the antibiotics, except for lomefloxacin, were greater than  
370 97% when the concentration of  $\text{Co}^{2+}$  further rose to 50  $\mu\text{g/L}$ . Kinetic investigations  
371 demonstrated that the destruction of antibiotics followed pseudo-first-order kinetics at the  
372 beginning 30 min. The obtained pseudo-first-order constants reveal that sulfisoxazole and  
373 trimethoprim were the easiest and most difficult compounds, respectively, to be degraded by  
374  $\text{Co}^{2+}$ -PMS (Fig. 6b).

375

#### 376 **4. Conclusions**

377 Trace levels of  $\text{Co}^{2+}$  were used as catalysts for PMS decomposition to degrade 1,4-D. The  
378 combination of PMS with  $\text{Co}^{2+}$  had a wide effective pH range (4.5 to 8.5); the pH value is  
379 typically found in the terrestrial environment. On the basis of the experimental observations,  
380 some conclusions can be drawn as follows:

381 (1) PMS could not obviously oxidize 1,4-D, and therefore unactivated PMS is inefficient to  
382 degrade 1,4-D;

383 (2) Rapid destruction of 1,4-D was observed when PMS co-presented with trace levels of  $\text{Co}^{2+}$ ;  
384 almost complete destruction was observed after reaction for only 6 min under the catalysis  
385 of 50  $\mu\text{g/L}$   $\text{Co}^{2+}$ ;

386 (3) Although trace levels of  $\text{Co}^{2+}$  could rapidly remove 1,4-D via catalysing PMS, their  
387 reactivity is quite limited during the mineralization;

388 (4) The destruction of 1,4-D was mediated by radicals, and  $\text{SO}_4^{\cdot-}$  was the dominant reactive  
389 species;

390 (5) Although pH 5.5 was the optimum condition for 1,4-D degradation, the best pH condition  
391 for the activation of PMS by Co<sup>2+</sup> was 7.0;  
392 (6) Compared with the other antibiotics investigated, ormetoprim, trimethoprim, and  
393 leucomycin were relatively more difficult to be oxidized by unactivated PMS;  
394 (7) Of the investigated antibiotics, lomefloxacin was the compound most difficult to be  
395 degraded by Co<sup>2+</sup>-PMS. The overall degradation rates of all the other antibiotics were  
396 greater than 97%.

397

398 **Acknowledgements**

399 This study was funded by the Research Grants Council of Hong Kong (Projects 106180082,  
400 C7044-14G, and T21-711/16R) and the start-up fund from South China Normal University  
401 (Project 8S0597).

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**List of Contents in Supporting Information**

568 **Table S1.** UPLC-(ESI<sup>+</sup>)-MS/MS conditions for the analysis of the selected antibiotics.

569 **Table S2.** Gradient program of the mobile phase.

570 **Figure S1.** Degradation of nitrobenzene by PMS alone or Co<sup>2+</sup>-PMS. Experimental conditions:

571 [nitrobenzene] = 0.1 mM, [PMS] = 2 mM. [Co<sup>2+</sup>] = 50 µg/L, and pH = 2.9 (original pH value).

572 **Figure S2.** Removal of TOC by Co<sup>2+</sup>-PMS. Experimental conditions: [1,4-D] = 5 mg/L, [PMS] = 2

573 mM, [Co<sup>2+</sup>] = 50 µg/L, and 5 mM phosphate buffer at pH 5.5.