

1 **High-efficiency Capture and Recovery of Anionic Perfluoroalkyl Substances**  
2 **from Water Using PVA/PDDA Nanofibrous Membranes with Near-zero**  
3 **Energy Consumption**

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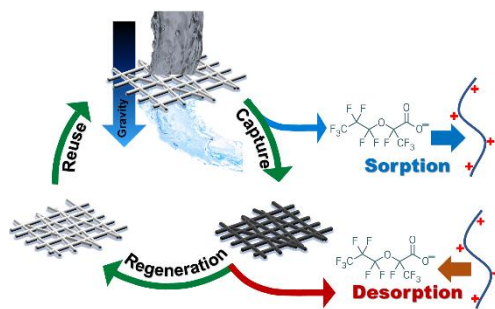
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26 ■ TABLE OF CONTENTS



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29 ■ **ABSTRACT**

30 Poly- and perfluoroalkyl substances (PFASs) have caused severe public concerns due to their  
31 toxicity and extensive occurrence in the aquatic environment. This study reports a highly porous  
32 amine-functionalized membrane for the rapid capture of GenX and other anionic PFASs (e.g.,  
33 perfluorooctane sulfonate (PFOS) and perfluorooctanoic acid (PFOA)) from contaminated  
34 water with near-zero energy consumption. The optimized membrane, prepared by  
35 electrospinning of polydiallyldimethylammonium chloride using crosslinked polyvinyl alcohol  
36 as a binder, had a high water permeability of  $\sim 2700 \text{ Lm}^{-2}\text{h}^{-1}\text{kPa}^{-1}$ . This high permeability  
37 enabled rapid gravity-driven filtration of contaminated water with a merely 5 cm water head,  
38 corresponding to an estimated energy consumption as low as  $2.7 \times 10^{-4} \text{ kWh/m}^3$ . Meanwhile, the  
39 membrane showed highly-efficient capture of GenX ( $> 97\%$ ), PFOS ( $> 99\%$ ), and PFOA ( $>$   
40  $99\%$ ). A large capture capacity of up to  $1.2 \times 10^6 \mu\text{g/m}^2$  was demonstrated for GenX. The  
41 captured GenX was recovered and concentrated with a small-volume NaCl/methanol solution,  
42 which simultaneously regenerated the membrane for its reuse. Over a 12-cycle capture-  
43 recovery test, the membrane demonstrated a high GenX recovery ratio of 94% and a volumetric  
44 concentration factor of 40. Our study provides a promising strategy for effective capture and  
45 recovery of GenX to enable its sustainable control and remediation.

46 ■ INTRODUCTION

47 Poly- and perfluoroalkyl substances (PFASs), such as perfluorooctane sulfonate (PFOS) and  
48 perfluorooctanoic acid (PFOA), have been widely detected in the environment and human  
49 bodies.<sup>1-6</sup> Because of their extreme persistence and toxicity,<sup>7-9</sup> PFOS and PFOA have been  
50 strictly regulated over the past decades<sup>10-12</sup> and have been replaced with short-chain PFASs in  
51 a number of industrial and commercial products.<sup>13, 14</sup> In recent years, the ammonium salt of  
52 hexafluoropropylene oxide dimer acid (HFPO-DA), commonly known as GenX and used as a  
53 main substitute chemical for PFOA, has been under public scrutiny and has been the subject of  
54 several major lawsuits related to drinking water contamination.<sup>15-19</sup>

55  
56 Recent toxicological investigations reveal that GenX has similar or even worse effects on the  
57 environment and human health compared to PFOA.<sup>20, 21</sup> Despite the quick actions by  
58 governments and manufacturers to curtail its discharge,<sup>22-24</sup> GenX is still continuously detected  
59 in the surface water with concentrations from several to hundreds ng/L.<sup>25, 26</sup> Urgent measures  
60 are called for to remediate GenX contamination for the protection of drinking water safety and  
61 public health.<sup>27, 28</sup> For example, its manufacturer, Chemours, has been mandated a minimal  
62 removal of 99% from its industrial waste effluent for subsequent destruction or reuse.<sup>29</sup> Treating  
63 GenX contaminated waters with low environmental concentrations yet huge volumes is a  
64 daunting challenge. Adsorption is able to remove GenX with some success while conventional  
65 sorbents such as activated carbon and resins requires extended treatment time (often due to  
66 mass transfer limitations).<sup>30</sup> On the other hand, advanced oxidation<sup>31</sup> or electrochemical

67 treatment<sup>32</sup> are highly energy intensive and are not suitable for treating large volumes of dilute  
68 streams. Highly efficient technology for the rapid capture and recovery of GenX is yet to be  
69 developed.

70  
71 This study reports a highly porous nanofibrous membrane with a nano-functionalized amine  
72 chemistry to separate GenX via an electricity- and chemical-free filtration. The large porosity  
73 of the membrane can enable rapid water transport even under gravity alone while the amine-  
74 based functionalization can realize effective removal of GenX due to their high affinity. A  
75 subsequent rinsing step was performed to recovery the enriched GenX for further destruction  
76 or recycle and to regenerate the exhausted membrane. Our study shows the feasibility of the  
77 rapid and effective remediation of water contaminated by GenX and other anionic PFASs using  
78 energy-efficient membrane separation.

79

## 80 ■ MATERIALS AND METHODS

81 **Chemicals.** Polyvinyl alcohol (PVA,  $n = 1700$ , i.e., the number of repeating units, TCI),  
82 polydiallyldimethylammonium chloride solution (PDDA, 20 wt.% in water, Sigma-Aldrich),  
83 and deionized (DI) water were used to prepare PVA/PDDA nanofibrous membranes by  
84 electrospinning. Acetic acid (99%, Dieckmann), glutaraldehyde (25 wt.% in water, Dieckmann),  
85 and hydrochloride acid (37%, VWR) were used to crosslink the membranes. GenX was  
86 received in the form of HFPO-DA (97%, Alfa Aesar). PFOA and PFOS were purchased from  
87 Sigma-Aldrich. The properties of GenX, PFOA, and PFOS were summarized in Table S1

88 (*Supporting Information S1*). Methanol (VWR) and sodium chloride (Uni-Chem) were used to  
89 prepare the rinsing solution for GenX recovery and membrane regeneration.

90

91 **Membrane fabrication and characterization.** PVA/PDDA nanofibrous membranes were  
92 fabricated using an electrospinning setup with three injection nozzles. For each membrane, a  
93 polymer dope solution was prepared by dissolving 10 wt.% PVA and 0-3.3 wt.% PDDA in DI  
94 water in a 90 °C water bath overnight. The dope solution was cooled to room temperature (~  
95 25 °C) and transferred to three 10 mL syringes (i.e., a total volume of 30 mL). Electrospinning  
96 was performed at a voltage of 18 kV, an injection rate of ~ 0.003 mL/min, a collection distance  
97 of 15 cm, and a receiving roller speed of 100 rpm. The electrospun membrane was subsequently  
98 immersed in the crosslinking solution containing 96 mL acetic acid, 4 mL glutaraldehyde, and  
99 0.1 mL HCl for a duration of 0.5 h. The crosslinked membrane was then thoroughly rinsed with  
100 DI water and stored in a DI water bath before further use. The fabricated membranes were  
101 designated as PDDA-0, PDDA-1, PDDA-2, and PDDA-3 according to their PDDA content of  
102 0, 1.0, 2.0, and 3.3%, respectively. Scanning electron microscope (SEM), elemental analyzer,  
103 and precision balance were used to characterize the morphology, structure, chemical  
104 composition, porosity, and grammage of the membranes (*Supporting Information S2*). At least  
105 three independent membrane samples were tested to determine membrane elemental  
106 composition, porosity, and grammage.

107

108 **GenX capture and recovery.** The capture of GenX was performed using a gravity-filtration

109 cell with an effective filtration area of 3.3 cm<sup>2</sup> (*Supporting Information S3*). A membrane  
110 coupon was placed in the cell followed by DI water rinsing. Subsequently, 2 L solution of GenX  
111 at a concentration of 200 µg/L was continuously introduced to the cell to implement gravity-  
112 driven filtration at a constant water head of 5.0 cm (corresponding to a hydrostatic pressure of  
113 0.49 kPa). A digital balance connected to a computer datalogging system was used to monitor  
114 the weight (and thus the volume) of permeate water collected as a function of time, and  
115 permeate samples were collected at specific volumetric intervals. Membrane regeneration and  
116 GenX recovery were performed for the PDDA-2 membrane over 12-cycle filtration tests to  
117 evaluate the durability of the membrane. At the end of each filtration cycle, the membrane was  
118 regenerated and the captured GenX was recovered by rinsing the membrane with a 50 mL  
119 mixture of 10 g/L NaCl and methanol with a volume ratio of 30/70%.<sup>33</sup> For comparison, the  
120 capture of PFOA and PFOS by the PDDA-2 membrane were also evaluated under identical  
121 operational conditions only the volume of feed solution was 4 L. The concentration of PFAS  
122 samples were determined by direct injection of samples into a liquid chromatography coupled  
123 with mass spectrometry (LC-MS) (*Supporting Information S4*).<sup>34</sup> The details of the calculation  
124 for membrane separation performance including water flux and capture ratio of PFAS as well  
125 as the recovery of GenX are described in *Supporting Information S5*.

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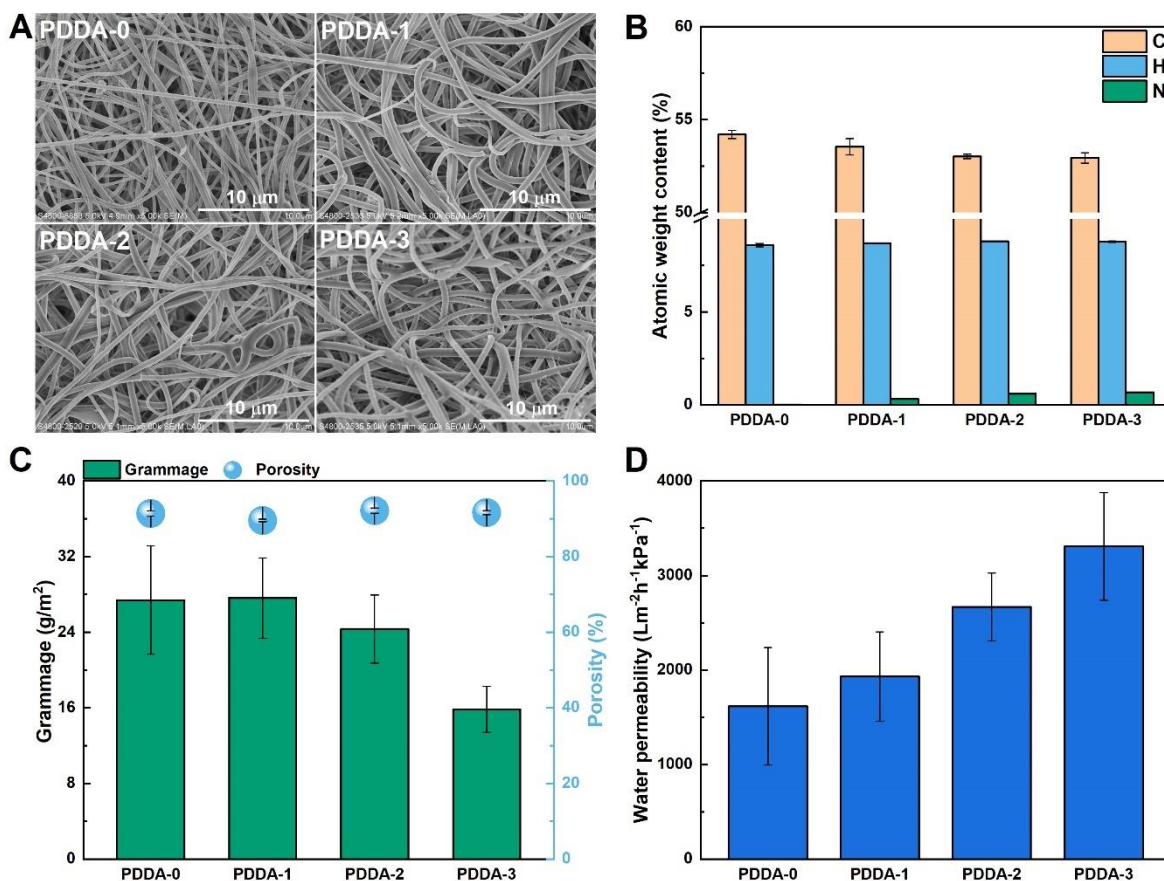
## 127 ■ RESULTS AND DISCUSSION

128 **Membrane characterization.** The electrospun membranes show typical nanofibrous structure  
129 consisting of a number of nanofibers, while the addition of PDDA has mild effect on membrane

130 morphology (Figure 1A). Elemental analysis reveals the presence of nitrogen in the PDDA-  
131 doped membranes (e.g., 0.3% for PDDA-1 to 0.6% for PDDA-3, Figure 1B), confirming the  
132 successful incorporation of PDDA. Membrane grammage (i.e., mass per unit membrane area)  
133 decreases with increasing the PDDA content (Figure 1C), which can be attributed to the reduced  
134 loading of nanofibers as a result of enhanced electrostatic repulsion.<sup>35</sup> According to the  
135 membrane grammage and the pre-determined weight content of PDDA in the membranes (i.e.,  
136 0-3.3 wt.%), the PDDA-2 membrane possessed the highest PDDA loading of 4.0 g/m<sup>2</sup> among  
137 all the membranes (*Supporting information S6*). All the membranes present high water  
138 permeability ranging from 1615 to 3308 Lm<sup>-2</sup>h<sup>-1</sup>kPa<sup>-1</sup> (Figure 1D), which is 3-4 orders of  
139 magnitude higher than that of typical gravity-driven membranes.<sup>36</sup> The high water permeability  
140 can attributed to the hydrophilic nature of the polymers (e.g., PVA and PDDA) and the high  
141 porosity of the membranes (e.g., ~ 90%, Figure 1C). Such high water permeability is beneficial  
142 for the rapid water production under gravity-driven condition (e.g., using a 5 cm water head in  
143 this study) and therefore enables near-zero energy filtration (e.g., corresponding to a specific  
144 energy consumption of 2.7×10<sup>-4</sup> kWh/m<sup>3</sup>, *Supporting Information S7*).

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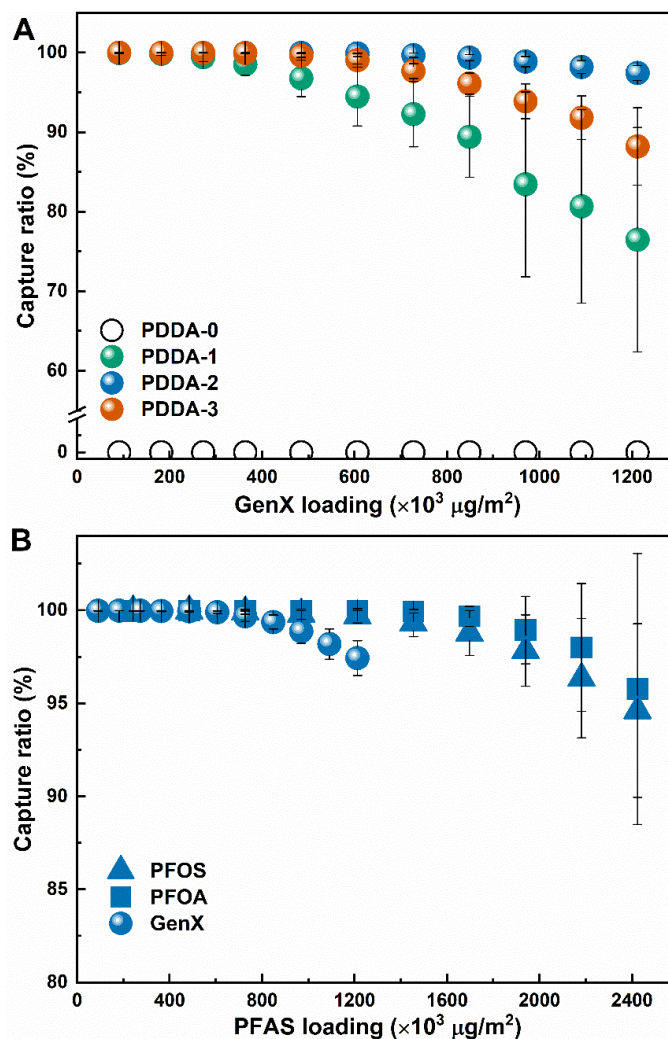
146  
 147 **Figure 1.** (A) SEM micrographs of membrane morphology, (B) elemental composition of C, H, and N, (C)  
 148 grammage (i.e., mass per unit membrane area) and porosity, and (D) water permeability for the various  
 149 PDDA membranes. The error bars represent the standard deviation acquired from at least three  
 150 independent samples.

151  
 152 **PFASs capture.** The blank membrane PDDA-0, which contained PVA only, had negligible  
 153 capture of GenX (Figure 2A). In contrast, the PDDA incorporated membranes (PDDA-1, 2, and  
 154 3) had progressive higher capture ratios at higher PDDA loadings, which reveals the critical  
 155 role of PDDA on the capture of GenX. This effect can be attributed to the electrostatic  
 156 attractions between the positively charged quaternary amine group in PDDA and negatively  
 157 charged carboxylic group in GenX.<sup>37</sup> The PDDA-2 membrane presented the highest capture  
 158 ratio of > 97% with the GenX loading up to  $1.2 \times 10^6 \mu\text{g}/\text{m}^2$ , which is partly due to its richest  
 159 content of PDDA among all the membranes (*Supporting Information S6*). Although PDDA-3

160 membrane also had high PDDA content, its capture ratio of GenX was lower than that of the  
161 PDDA-2 membrane, which may be attributed to the reduced residence time of GenX within the  
162 PDDA-3 membrane as a result of its high water permeability (Figure 2D). The capture ratio of  
163 GenX by filtration was significantly higher than that by adsorption with same treatment time  
164 (Figure S4, *Supporting Information S8*), which can be attributed to the greatly improved mass  
165 transfer in the “flow-through” filtration mode. Similar enhancement effects of “flow-through”  
166 over “flow-by” have been observed in the context of catalysis.<sup>38</sup> In addition to GenX, the  
167 PDDA-2 membrane also presented excellent capture efficiency for PFOS and PFOA (Figure  
168 2B). The capture ratio of PFOS and PFOA remained at ~ 95% with the PFOS or PFOA loading  
169 up to  $2.4 \times 10^6 \mu\text{g}/\text{m}^2$ . Although PFOS and PFOA has been replaced by short-chain PFAS (e.g.,  
170 GenX) for decade, their occurrence in the water system are continuously reported.<sup>39, 40</sup> Our  
171 results demonstrate the great potential of the PDDA membranes for highly efficient capture of  
172 PFASs (e.g., PFOS, PFOA, and GenX) from contaminated water. In addition to the capture of  
173 single PFAS, we also evaluated the ability of the PDDA-2 membrane for capturing GenX,  
174 PFOA, and PFOS from their mixed solution containing  $10 \mu\text{g}/\text{L}$  for each compound (*Supporting*  
175 *Information S9*). For volumetric loading of up to  $6000 \text{ L}/\text{m}^2$ , the membrane showed high capture  
176 ratios of  $\geq 99\%$  for all three PFASs (Figure S5). With the increase of volumetric loading, the  
177 capture ratio of GenX was reduced and those of PFOS and PFOA remained stable. This result  
178 is consistent with Figure 2B and other published literature,<sup>33</sup> which can be attributed to the  
179 lower affinity of GenX to amine-based functional groups compared to PFOS and PFOA  
180 (*Supporting Information S10*). Nevertheless, the capture ratio of GenX remained at  $> 92\%$  with

181 a volumetric loading up to  $\sim 9000$  L/m<sup>2</sup> (Figure S5).

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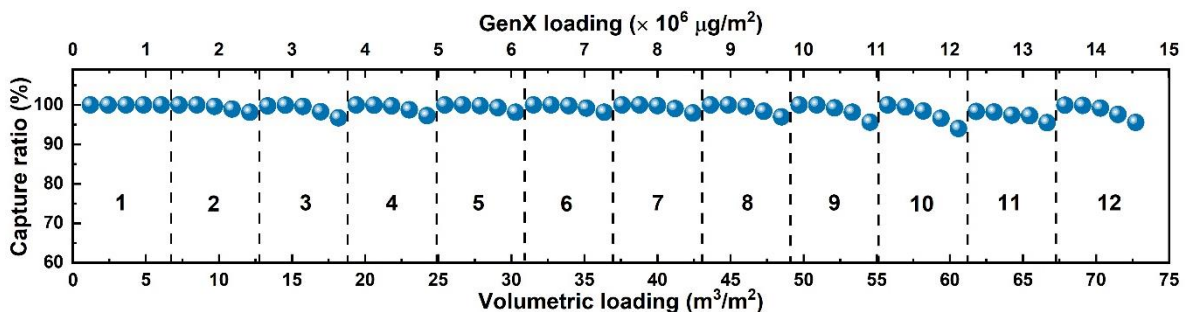
183  
184 **Figure 2. (A) The capture ratio of GenX as a function of GenX loading for the various PDDA membranes,**  
185 **and (B) the capture ratio of PFOS, PFOA, and GenX for the PDDA-2 membrane. Experimental conditions:**  
186 **2 L feed solution containing 200  $\mu\text{g}/\text{L}$  GenX, effective membrane filtration area of 3.3 cm<sup>2</sup>, water head of 5.0**  
187 **cm. For the capture of PFOA and PFOS, the volume of feed solution was 4 L while other experimental**  
188 **conditions were identical. The error bars represent the standard deviation acquired from at least three**  
189 **independent samples.**

190

191 **GenX recovery and membrane regeneration.** Following the effective capture of GenX from  
192 a contaminated water, its subsequent recovery is also critical for the potential destruction or  
193 recycle of the compound as well as the sustainable reuse of the membrane. A simple rinsing

194 using NaCl/methanol solution was performed to simultaneously extract the captured GenX and  
 195 to regenerate the membrane. As shown in Figure 3, the PDDA-2 membrane maintained high  
 196 capture ratio of GenX (e.g., > 95%) over the 12 capture-recovery cycles, suggesting the  
 197 successful regeneration of the membrane. Since the used membrane was regenerated by only  
 198 50 mL NaCl/methanol solution after treating 2 L solution of 200  $\mu\text{g/L}$  GenX, a high volumetric  
 199 concentration factor of 40 was achieved for the GenX recovery. Meanwhile, 94.0% of the GenX  
 200 in the feed water was recovered from the membrane and concentrated in the small-volume  
 201 rinsing solution. The highly effective capture, recovery, and concentration of GenX enables its  
 202 further destruction or reuse in a centralized way, which can significantly reduce the overall  
 203 treatment cost while improving the efficiency.

204



205

206 **Figure 3. The capture ratio of GenX by PDDA-2 membrane over 12 capture-recovery cycles. Experimental**  
 207 **conditions: 2 L feed solution containing 200  $\mu\text{g/L}$  GenX, effective membrane filtration area of 3.3  $\text{cm}^2$ , water**  
 208 **head of 5.0 cm. At the end of each filtration cycle, 50 mL mixture of 10 g/L NaCl and methanol with a volume**  
 209 **ratio of 30/70% was added into the cell to recover the captured GenX and regenerate the membrane.**  
 210 **Subsequently, 50 mL DI water was added into the cell to rinse the membrane for next filtration cycle. Total**  
 211 **12-cycle filtration tests were performed.**

212

213 The global occurrence of GenX poses daunting threats to the environment and public health.<sup>2,</sup>

214 <sup>20, 25</sup> A recent study by Joerss et al. revealed the transport of GenX far to the remote Arctic

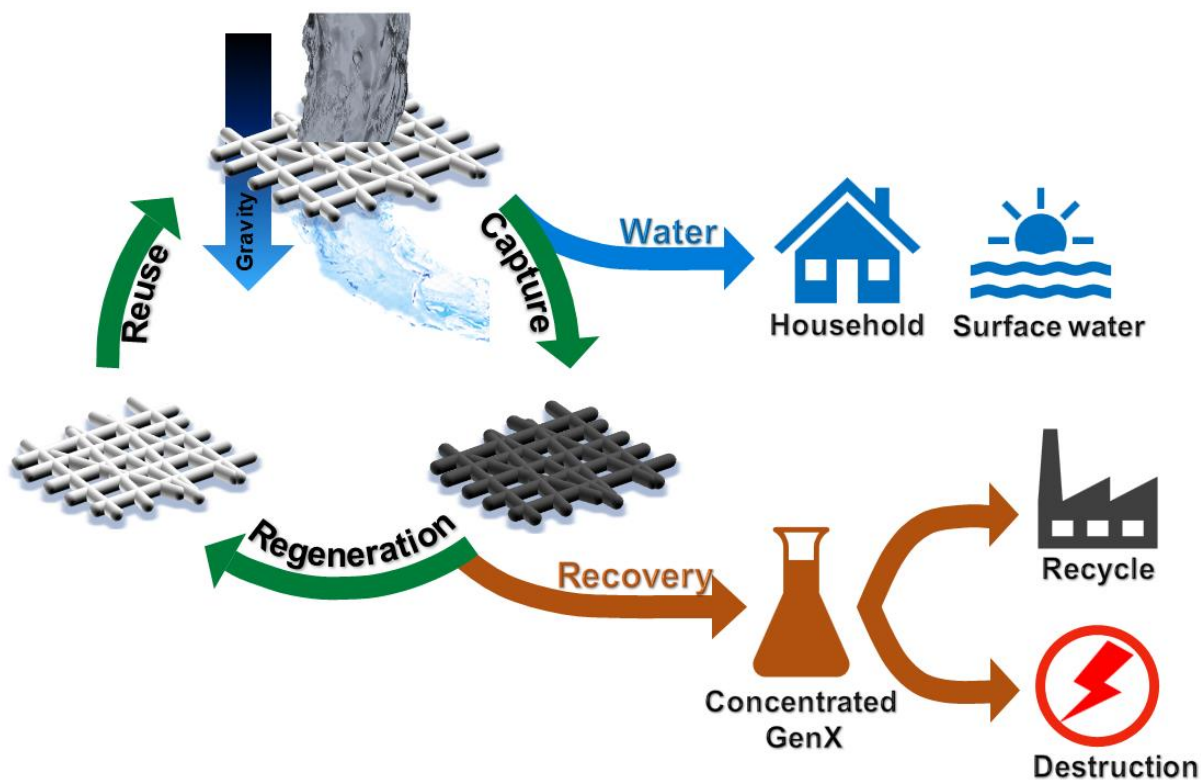
215 Ocean,<sup>41</sup> which presents alarming evidence for the wide spread of GenX contamination.  
216 Effective control and remediation strategies are urgently called to prevent the further discharge  
217 of GenX into the environment as well as to remove it from the contaminated waters. Our study  
218 presents a sustainable membrane filtration technology to address this critical issue through (1)  
219 the effective capture of GenX from a large-volume contaminated water using a gravity-driven  
220 PDDA nanofibrous membrane, and (2) its concentration and recovery for further destruction or  
221 recycle (Figure 4). In addition, the rapid filtration process requires no electricity input, which  
222 may be used in remote areas or in underdeveloped regions and offers significant advantages  
223 over other technologies (e.g., electrochemical degradation).<sup>32</sup> Meanwhile, the sustainable reuse  
224 of the membrane also effectively reduces the operational cost.

225

226 To control the discharge of GenX from the industrial sources, one can further implement a  
227 multi-pass filtration to ensure a high overall capture efficiency of > 99% that has been mandated  
228 in some countries.<sup>29</sup> The captured GenX can be recovered for further reuse or treatment within  
229 the manufacturing site and thus curtails its transport to the environment. For the removal of  
230 GenX from contaminated surface waters, the gravity-driven filtration technology can be  
231 integrated into the existing water treatment chains as a polishing step.<sup>36</sup> Alternatively, it can  
232 potentially be used as a point-of-use treatment technology for the decontamination of GenX in  
233 household (e.g., tap waters or groundwaters).<sup>42</sup> To enable such practical applications, future  
234 studies need to systematically investigate membrane separation performance under a wider  
235 range of feed water qualities as well as the effect of biofilm growth and membrane fouling on

236 the removal efficiency.<sup>36</sup> The novel filter can also be potentially used for the removal of other  
237 anionic PFASs.

238



239  
240 **Figure 4. Illustration of the proposed gravity-driven membrane filtration technology for the sustainable**  
241 **capture and treatment of GenX.**

242

## 243 ■ ASSOCIATED CONTENTS

244 **Supporting Information.** S1. Properties of GenX, PFOA, and PFOS; S2. Membrane  
245 characterization; S3. Gravity-driven filtration setup; S4. LC-MS analysis for PFASs; S5.  
246 Calculation of water permeability, capture ratio, and recovery ratio; S6. PDDA content of the  
247 membranes; S7. Specific energy consumption; S8. Comparison between filtration and  
248 adsorption; S9. Membrane separation performance for mixed PFASs; S10. Binding affinity of  
249 PFASs with PDDA membranes; S11. Effect of organic matter on the removal of GenX; S12.

250 Comparison between the PDDA-2 membrane and SPE cartridge; S13. Membrane pore size.

251 This material is available free of charge at <http://pubs.acs.org>.

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### 258 Notes

259 The authors declare no completing financial interest.

260

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268



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